

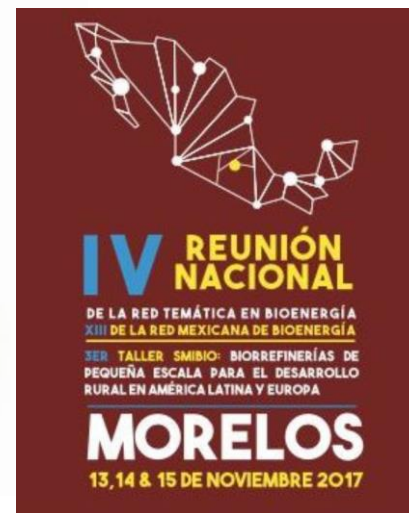
MICROBIAL FUEL CELLS

Aprovechamiento del potencial energético de sedimentos contaminados con hidrocarburos

Using anode-respiring bacteria to generate direct electrical current from hydrocarbon sediments

Dra Katy Juárez López

Departamento de Ingeniería Celular y Biocatálisis.
Instituto de Biotecnología, UNAM.



BIOENERGY AND ENVIRONMENT

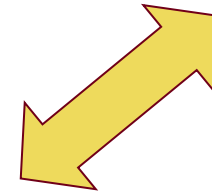
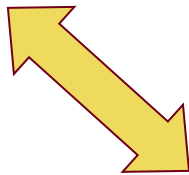
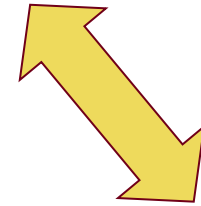
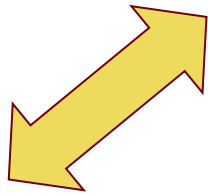
**Bioelectricity: Bioelectrochemical Systems
BES**

**ELECTRON TRANSFER
PROCESSES**

Bioremediation
Heavy metals

Isolation of microorganism
with novelty capabilities

Hydrocarbon degradation (BES)

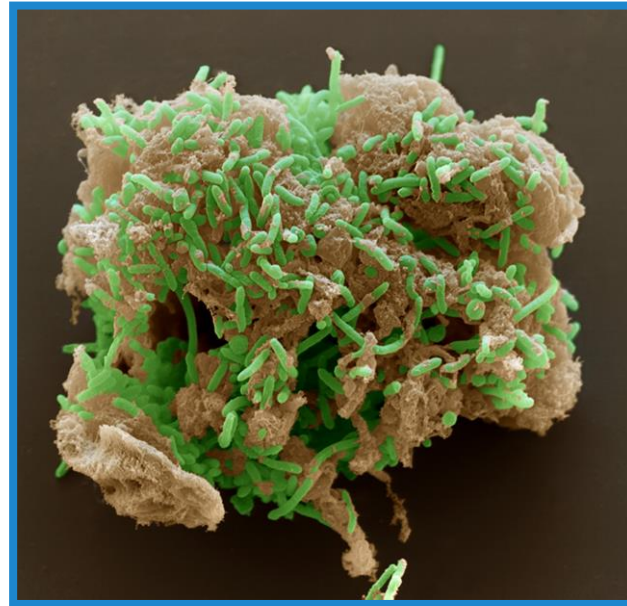
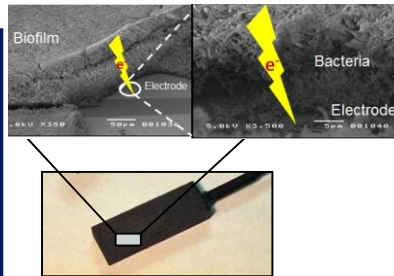


Geobacter sulfurreducens: model bacteria for extracellular electron transfer

bioelectricity

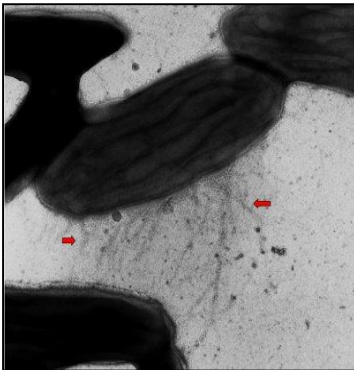


Microbial Fuel Cell (MFC)

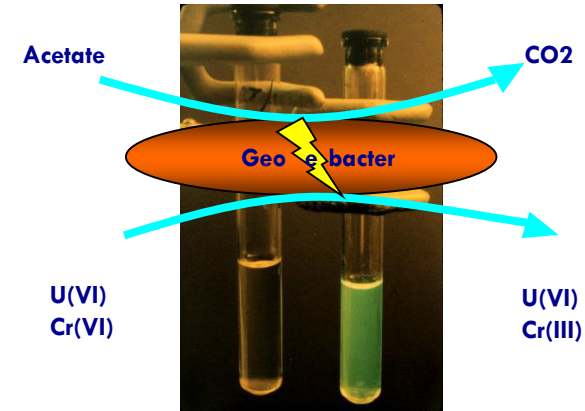


- Subsurface bacteria, anaerobic
- Biogeochemical cycles Fe and Mn.
- Electron transfer to extracellular insoluble acceptors.
- More than 100 cyt

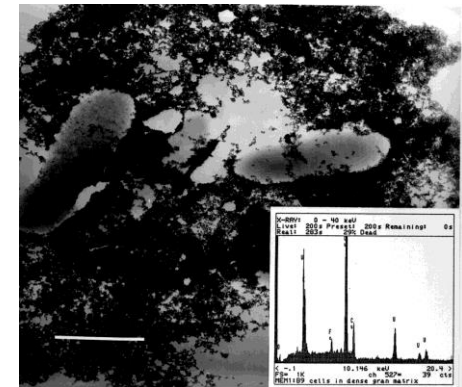
Geopili "nanocables"



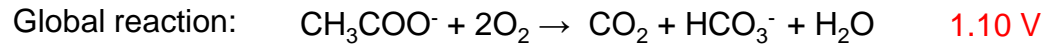
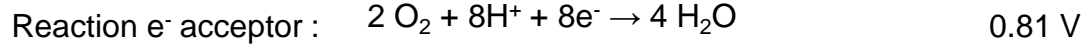
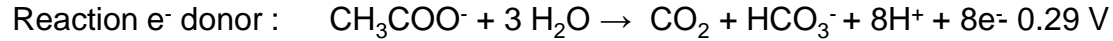
Bioremediation



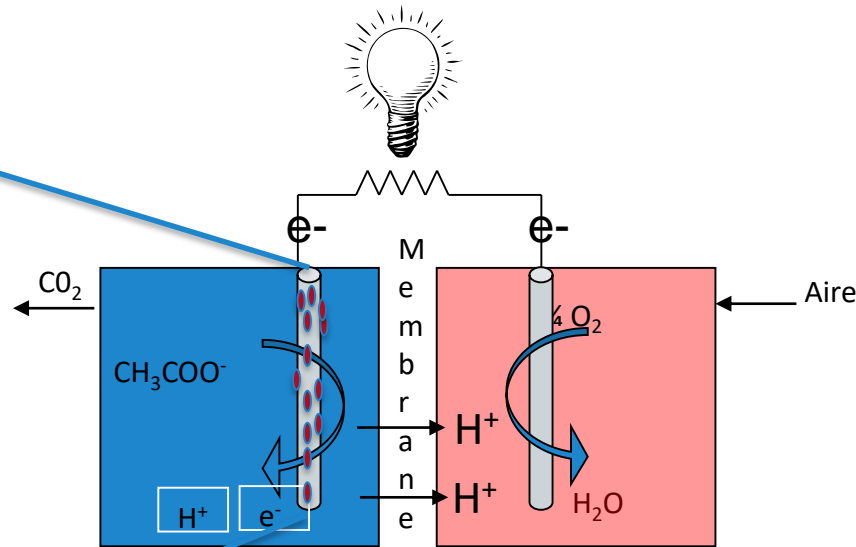
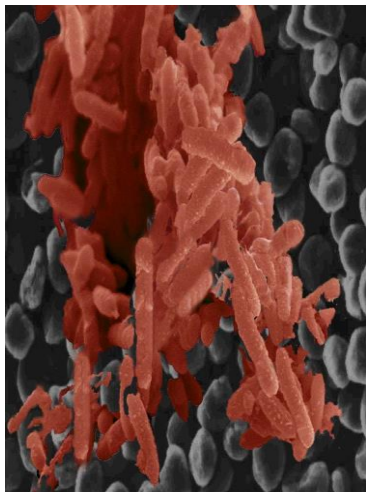
Hydrocarbon degradation



Microbial Fuel Cell



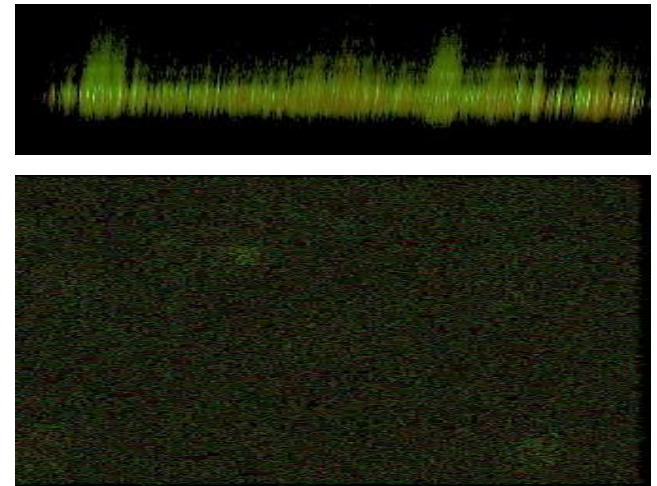
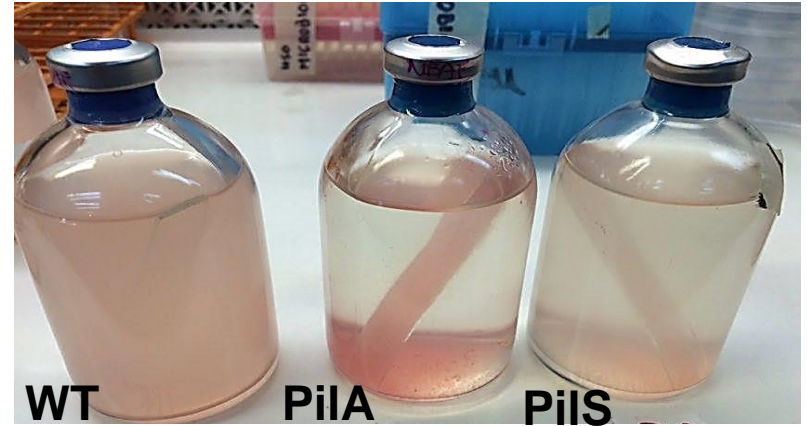
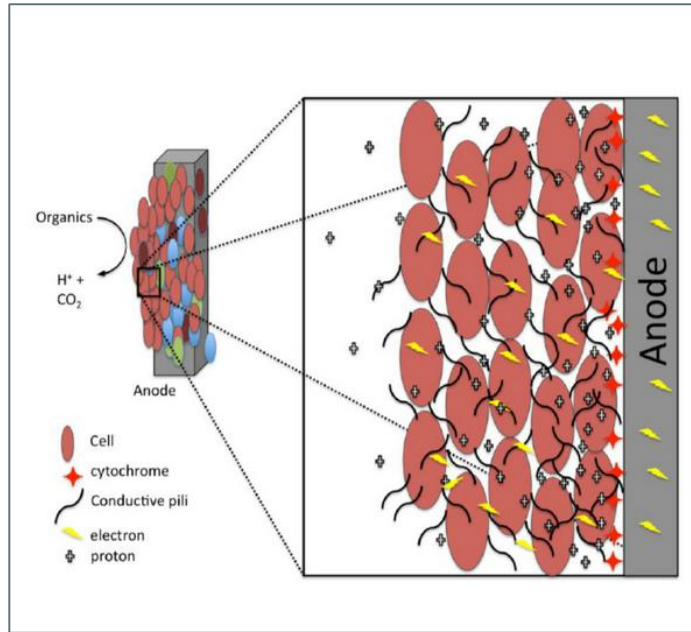
↓
0.3 - 0.6 V



What is the limiting factor ?

- BIOFILM (electron transfer)
- Anode material and architecture MFC
- Inhibiting metabolites
- Internal resistance

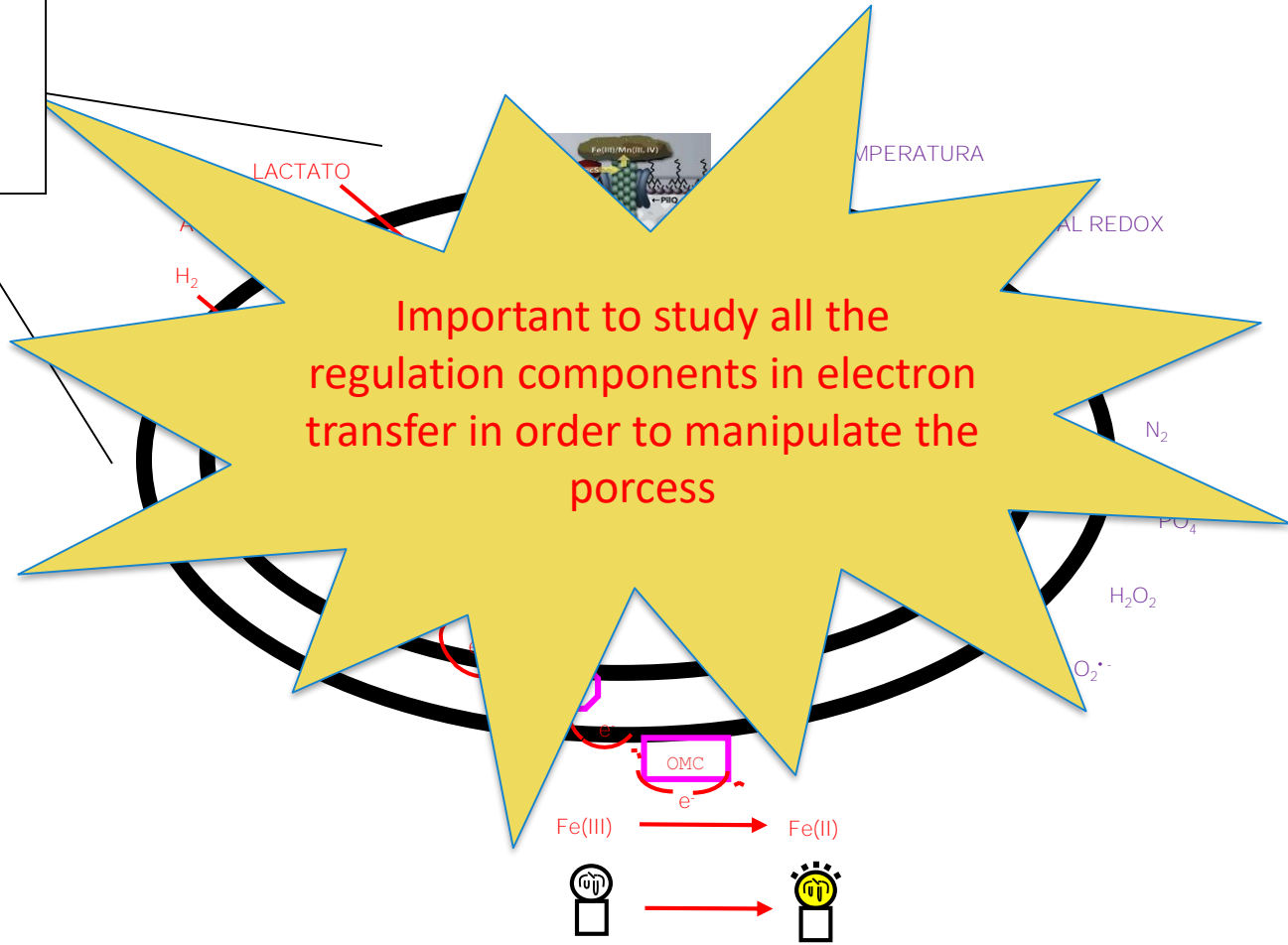
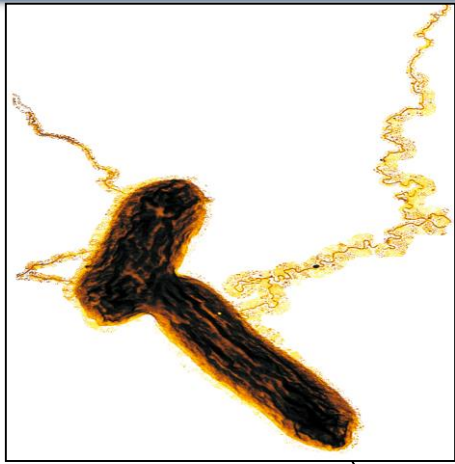
Biofilm characterization in MFC



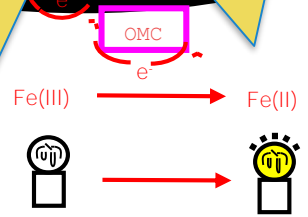
Mutant PilA-
Biofilm non
conductive



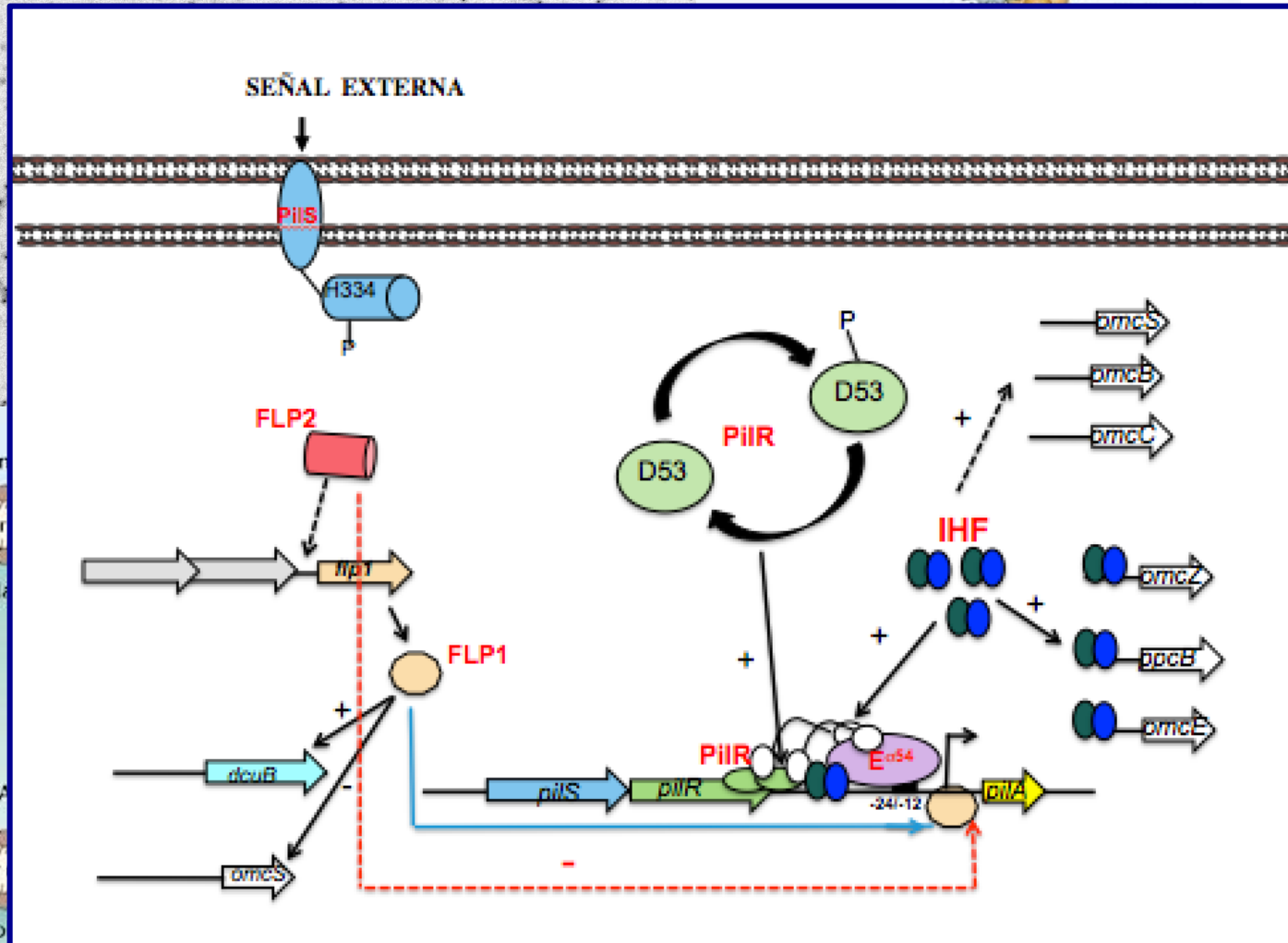
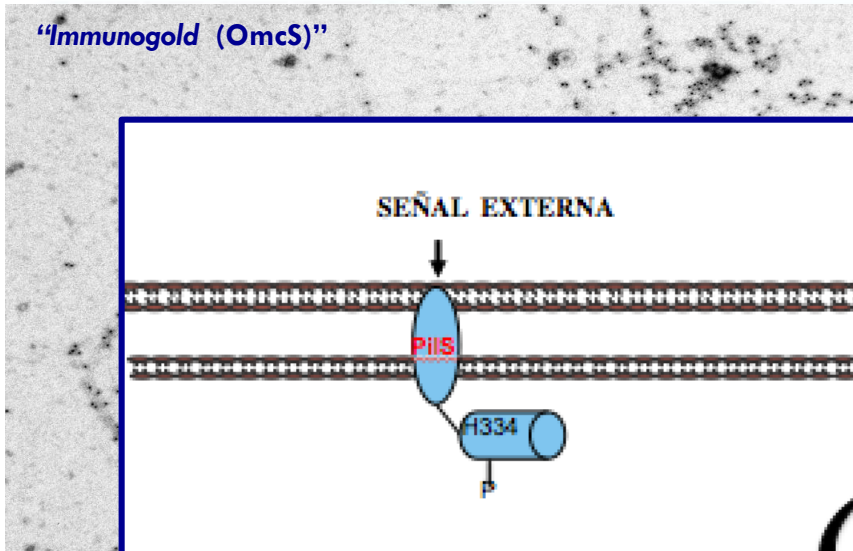
ELECTRON TRANSFER REGULATION Fe(III) other heavy metals and anode in MFC?



Important to study all the regulation components in electron transfer in order to manipulate the process



¿Cómo se lleva a cabo la transferencia de electrones?



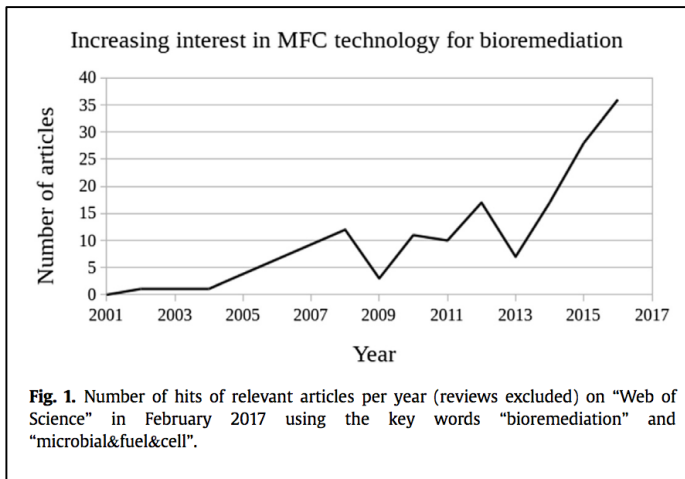
proteína estructural
pili

modificado de Lovley. 2006. *Nat Rev Microbiol* 4, 497

Leang, et al. 2010. *Appl Environ Microbiol* 76, 4080

Rollefson, et al. 2011. *J. Bacteriol* 193:1023-33

BES IN BIOREMEDIATION AND OTHER PROCESS

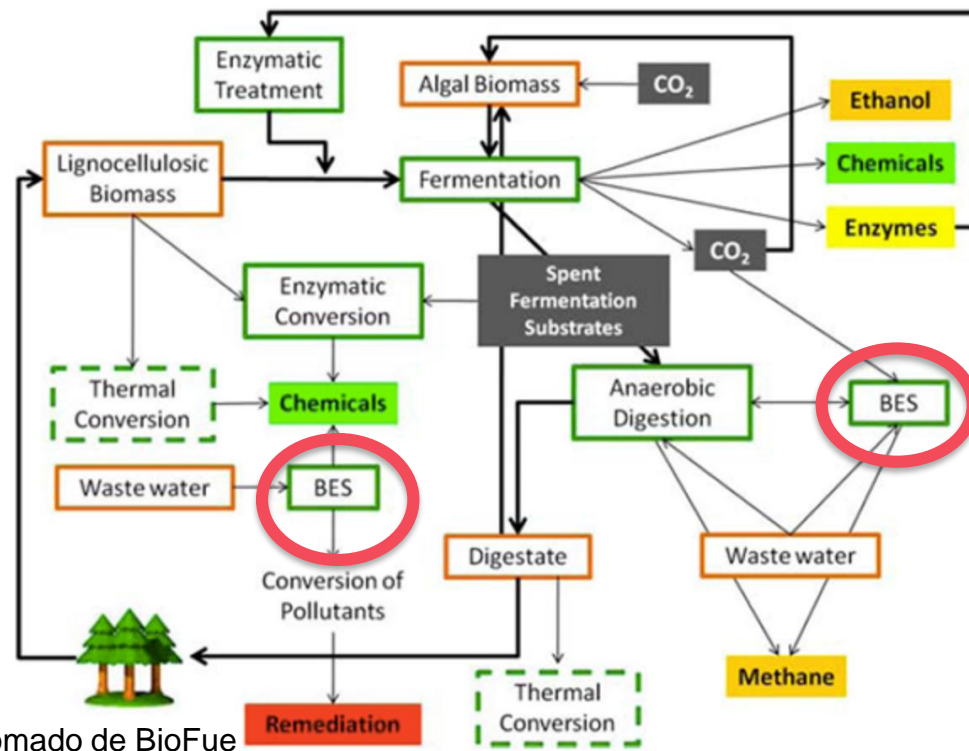


M. Kronenberg et al. / Environmental Pollution 231 (2017) 509-523

a) Early MFC System Cost in \$/m ²		b) MFC Cost with New Materials in \$/m ²	
	Cost		Cost
Carbon Cloth	~ \$1000	Anode	~ \$20
Platinum Catalyst	~ \$500	Cathode	~ \$22
Binder	~ \$700	Binder	~ \$1.50
Diffusion Layer	~ \$0.30	Activated Carbon [cathode/catalyst]	~ \$0.40
Separator	~ \$1.00	Diffusion Layer	~ \$0.15
Total	~\$2200	Separator	~ \$1.00
		Total	~ \$43

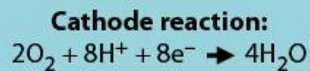
Table 1: a) Breakdown of early MFC costs for materials in \$/m² (USD), b) Breakdown of MFC costs using more recent and cost-effective materials. Adapted from [169,170].

Biorefineries



Producción de electricidad de sedimentos acuáticos y desechos orgánicos

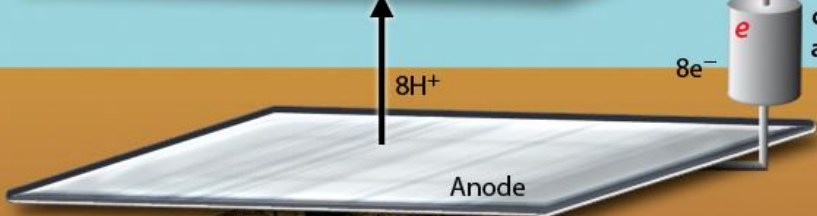
Microbial Fuel Cell



Cátodo aeróbico

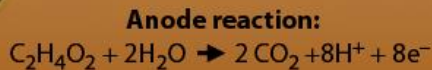
Electrons flow to cathode, creating an electrical current.

Water
Sediment

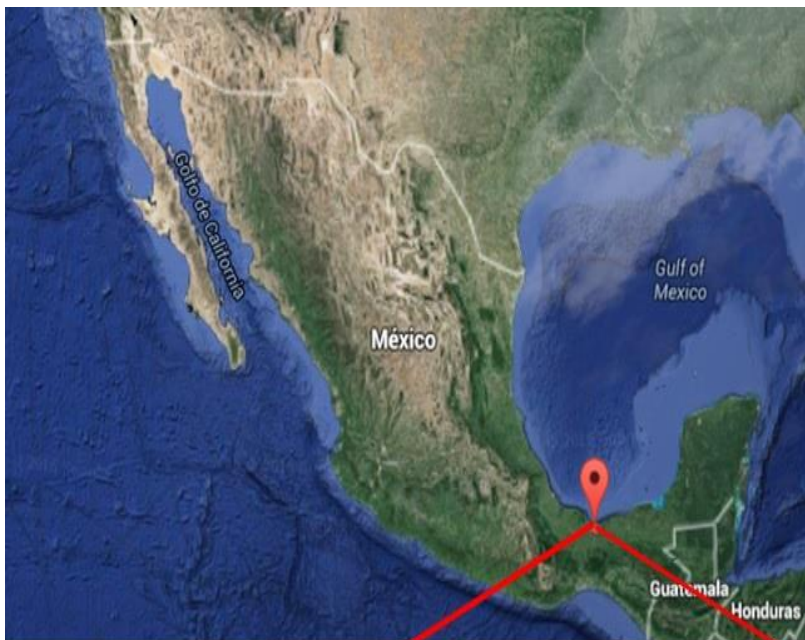


Ánodo anaeróbico

Biofilm of *Geobacter* cells on anode surface revealed with scanning electron microscopy



ISOLATION OF MICROBIAL CONSORTIA METAL REDUCERS AND HYDR DEGRADERS



BACTERIAL DIVERSITY 16s DNAr

MICROORAGANISMO	Identidad
<i>Geobacter</i> sp. Strain AK14	96%
<i>Geobacter</i> sp. Strain G02	99%
<i>Geobacter</i> sp. Strain CdA-3	99%
<i>Petrinomonas</i> sp. Strain B50-1	99%
<i>Clostridium</i> sp. Strain AP	99%
<i>Clostridium amygdalinum</i> strain 48AGP6	95%
<i>Porphyromonas</i> sp. HCB-7	95%
<i>Geobacter</i> sp. Strain CdA-3	92%

Fe(III) as electron acceptor : acetate and HYD as electron donor.

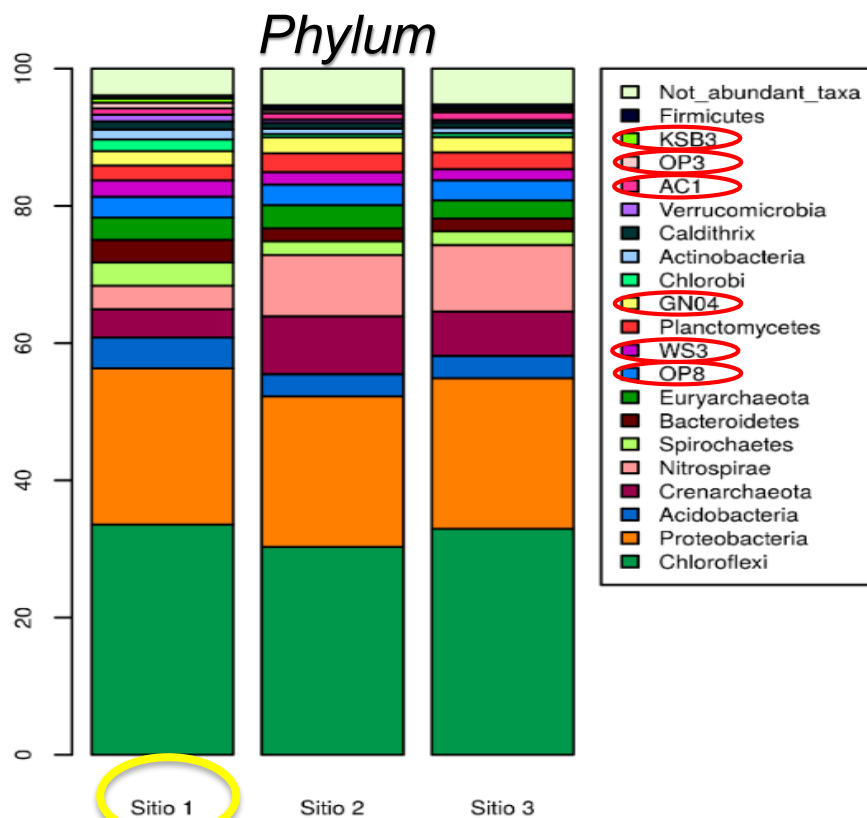


HEAVY METALS SITE 1

	U (ppm)	Pb (ppm)	Tl (ppm)	Hg (ppm)	Cr (ppm)	Mn (ppm)
SED. SITIO1	0.8	9.3	0.27	120	40.8	300

Limite permisible de Hg en sedimento (OMS) 0.1ppm

MICROBIAL DIVERSITY COATZACOALCOS RIVER



Amplicon 16s rDNA (V3-V4). Taxonomic Assignment Phylum level

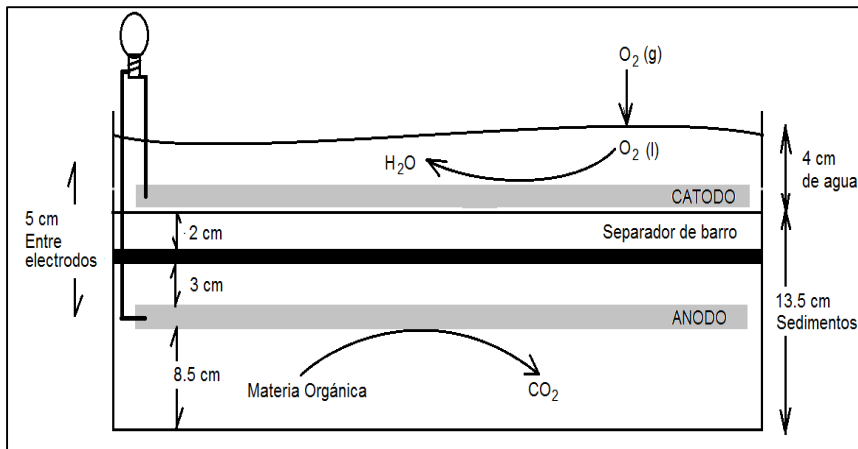
Candidato a Phylum	Procedencia
KSB3 (Tanner <i>et al.</i> , 2000)	biorreactor anaeróbico de tratamiento de aguas residuales.
OP3 (<i>Omnitrophica</i>) (Stevens <i>et al.</i> 2008)	Sedimentos marinos con baja concentración de oxígeno.
AC1 (Harris <i>et al.</i> , 2004)	Sedimento marino, birreactor de desnitrificación
GN04 (Narihiro <i>et al.</i> , 2015)	Sedimentos marinos, planta tratadora de efluentes industriales
WS3 (Dojka <i>et al.</i> , 1998)	Acuífero contaminado con hidrocarburo y compuestos clorados
OP8 (<i>Aminicenantes</i>) (Frag <i>et al.</i> , 2014)	Sedimentos acuáticos contaminados con hidrocarburos

Amplicon 16s rDNA (V3-V4). Taxonomic Assignment Genera level

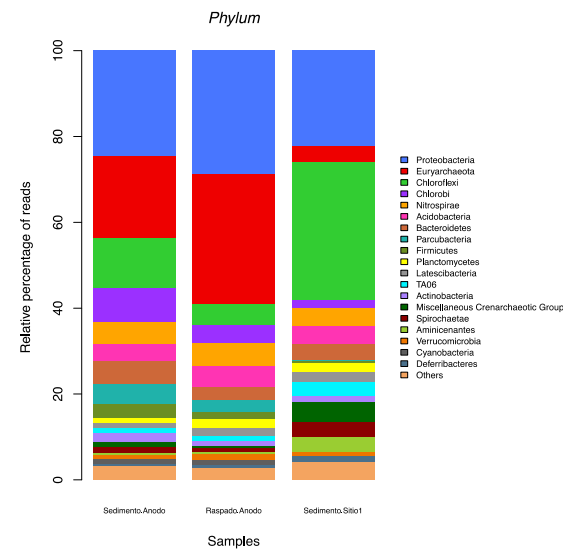
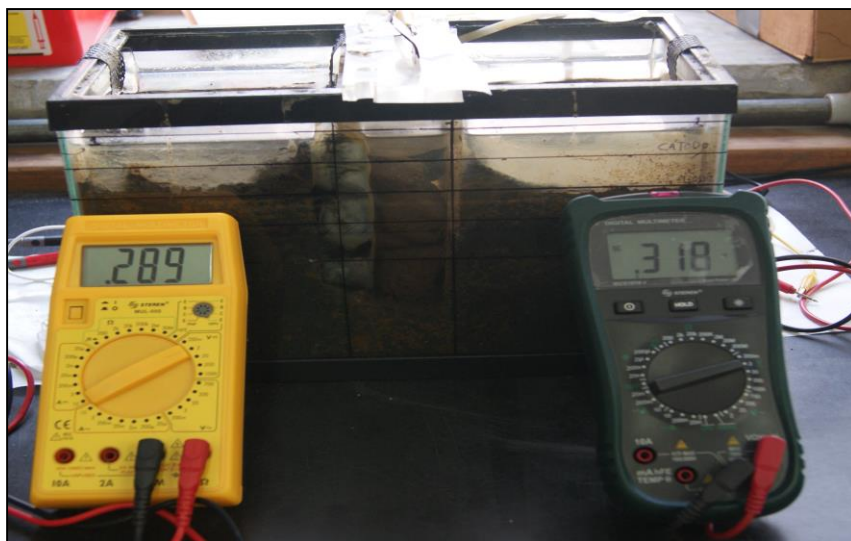
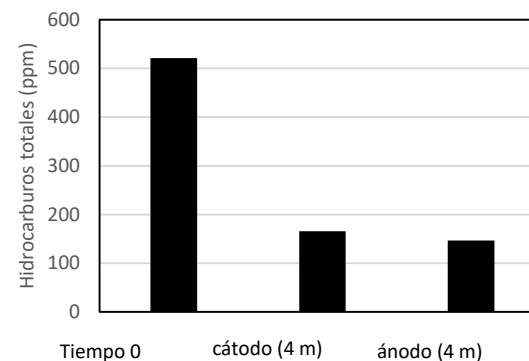
Clona	Procedencia
GOUTA19 (Alfreider <i>et al.</i> , 2002)	Aguas contaminadas con mono-clorobenceno
SJA-88 (Wintzingerode, 1999)	Sedimento en hidrocarburos aromáticos policíclicos
LCP-26 (Kostka <i>et al.</i> , 2004)	Sedimento marino contaminado mercurio e hidrocarburo
LCP-6 (Kostka <i>et al.</i> , 2004)	Sedimento marino contaminado mercurio e hidrocarburo

BIOELECTROCHEMICAL SYSTEM: SEDIMENTS SITE 1 COATZACOALCOS

BES : MATERIALS LOW COST

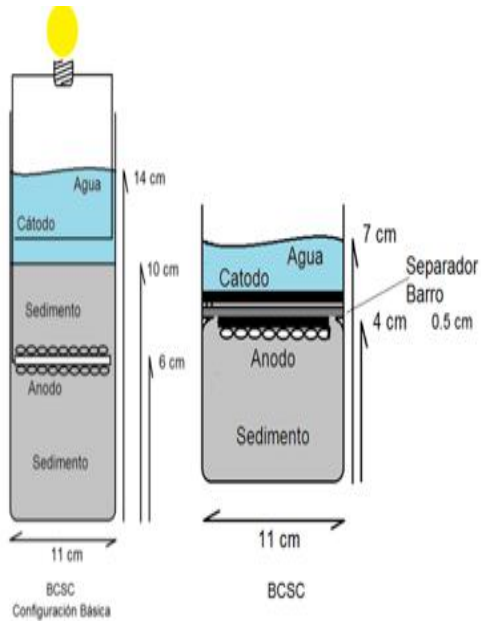


TOTAL HYDROCARBON DEGRADATION

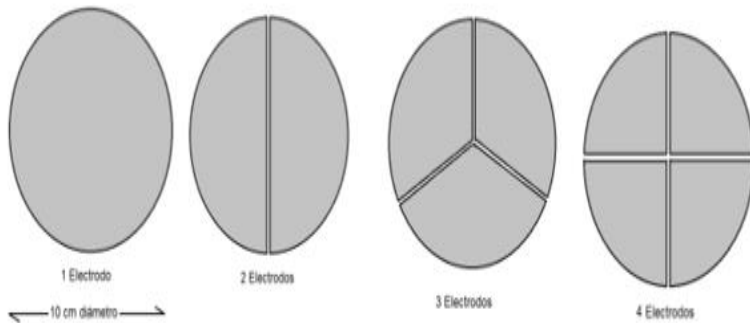
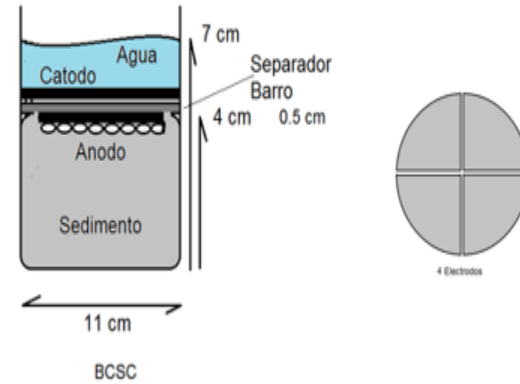


DIFFERENT ARCHITECTURE IN BES AND ANODES

2
a



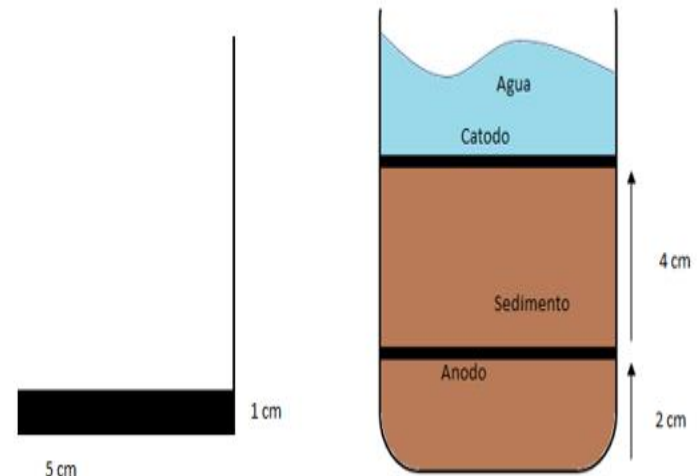
3c4s



3c1s
3c4s

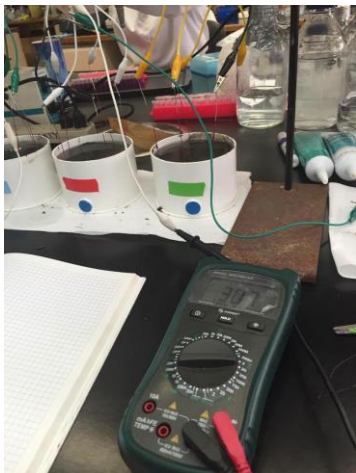
3c2s

3c3s



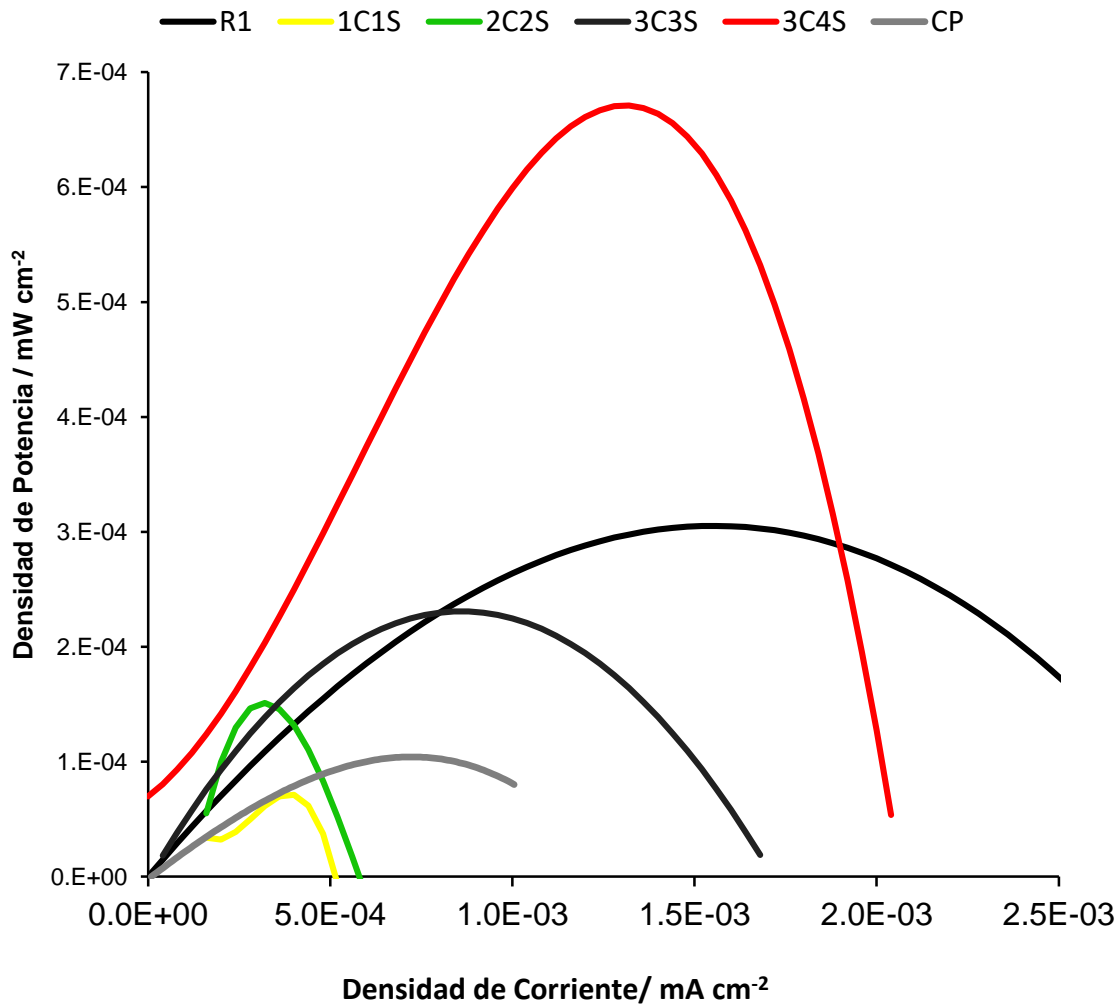
A,B,C Y D

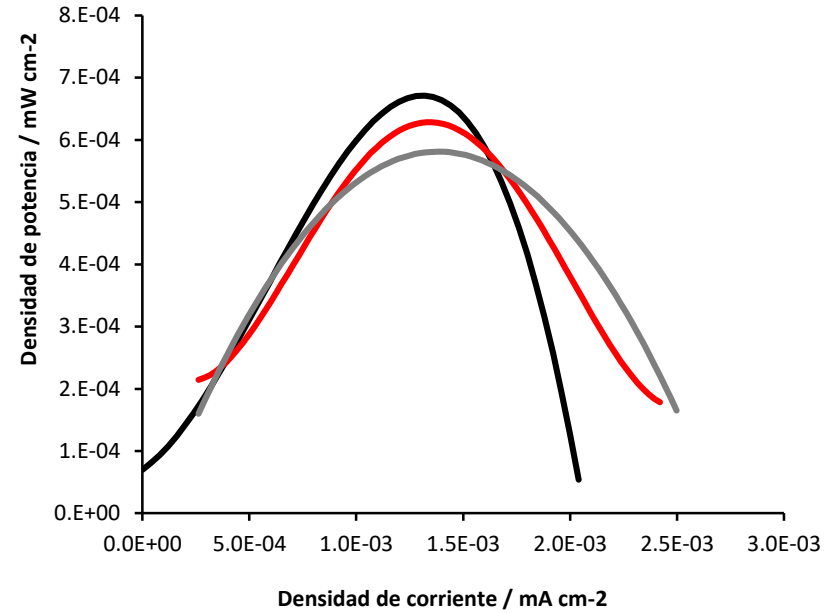
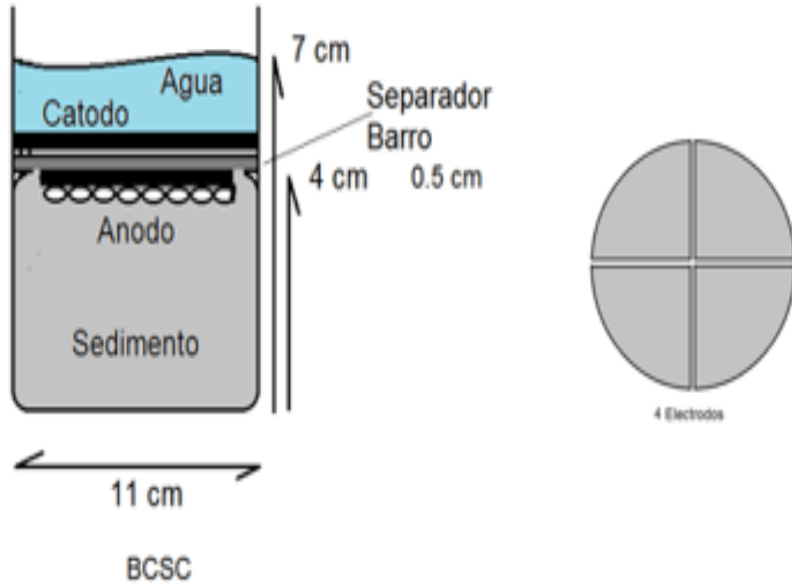
POWER DENSITY OF DIFFERENT CELLS



DP
1C1S $\rightarrow 7.48 \cdot 10^{-5} \text{mW/cm}^2$

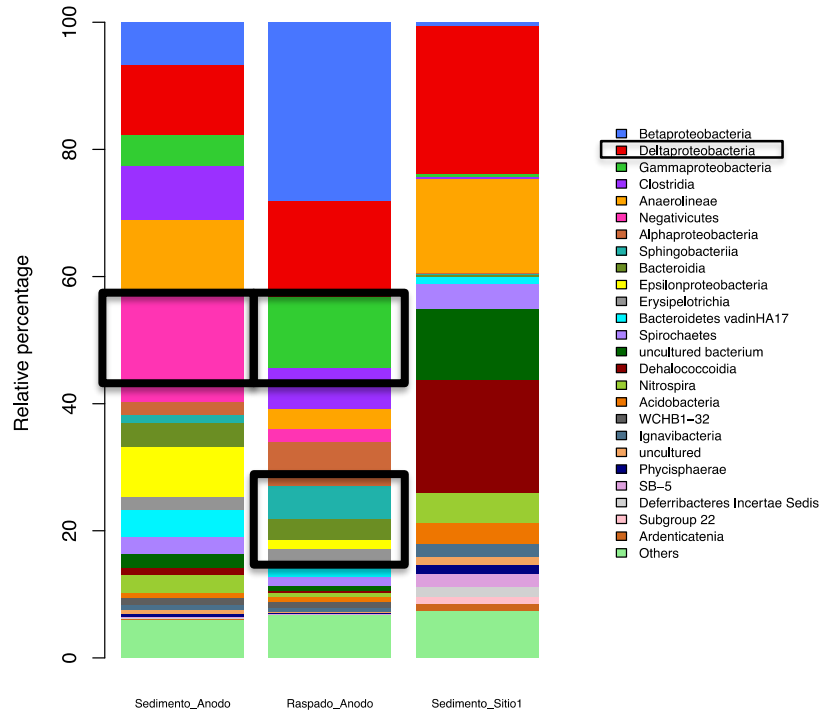
4C4S $\rightarrow 6.80 \cdot 10^{-4} \text{mW/cm}^2$



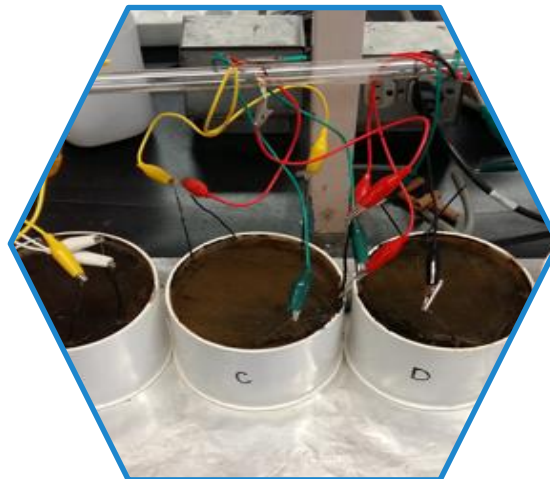
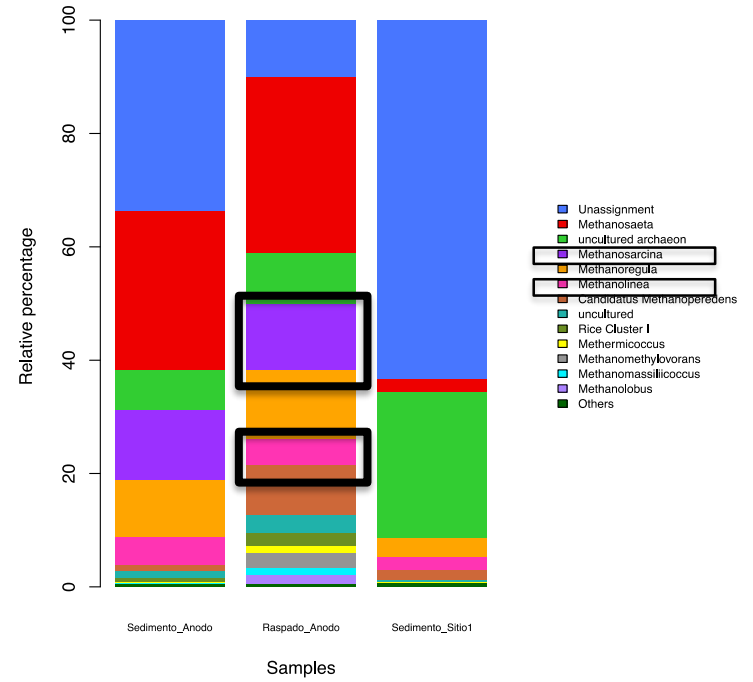


BCM	Sustrato Anolito	Área y Material Ánodo	Área Cátodo CF	Modificación Cátodo	Dist Elect	Separador	PCA V	Resist Interna Ω	DC Max mA cm^{-2}	DP Max mW cm^{-2}
3c 4s	Sedimento sitio 1	4 CF Seg 0.00785 m^2	0.00785 m^2	Sin Modificación	0.005 m	Barro	0.67	1195	1.5×10^{-3}	6.8×10^{-4}

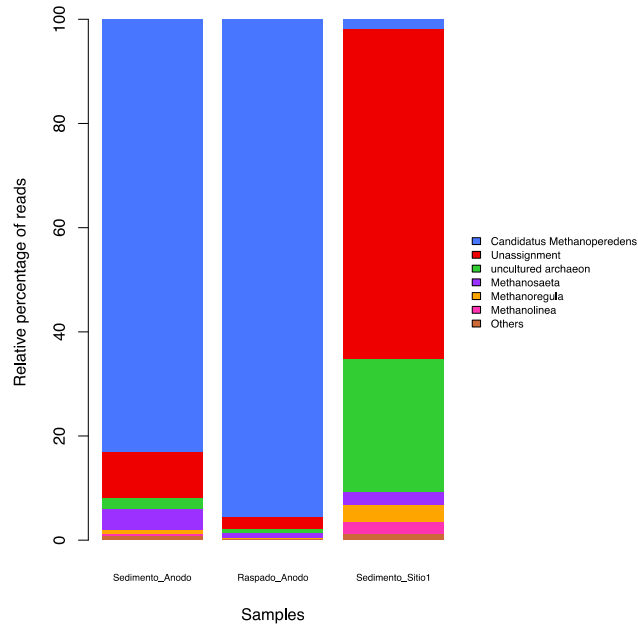
Class Bacterias



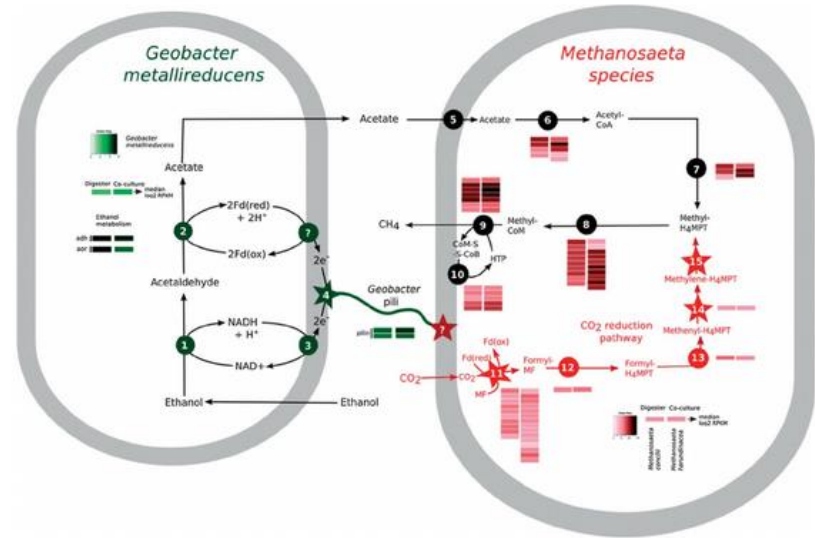
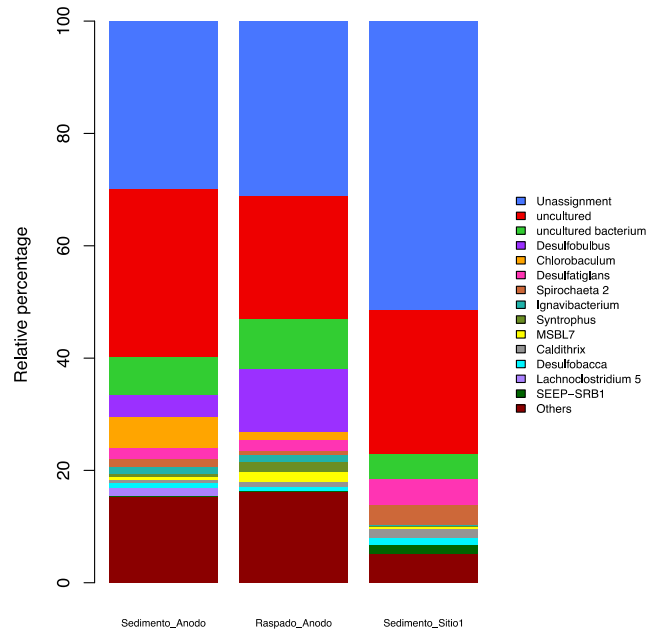
Genus Archaeas



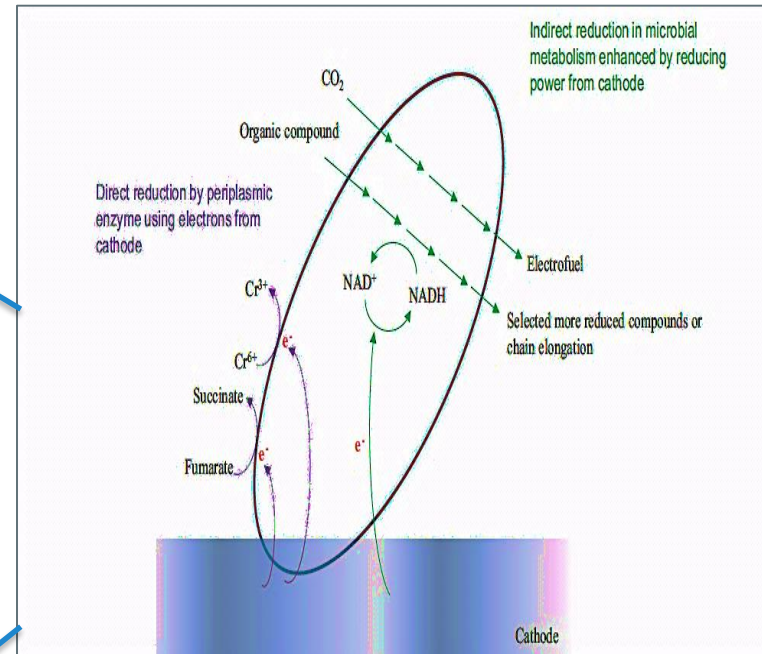
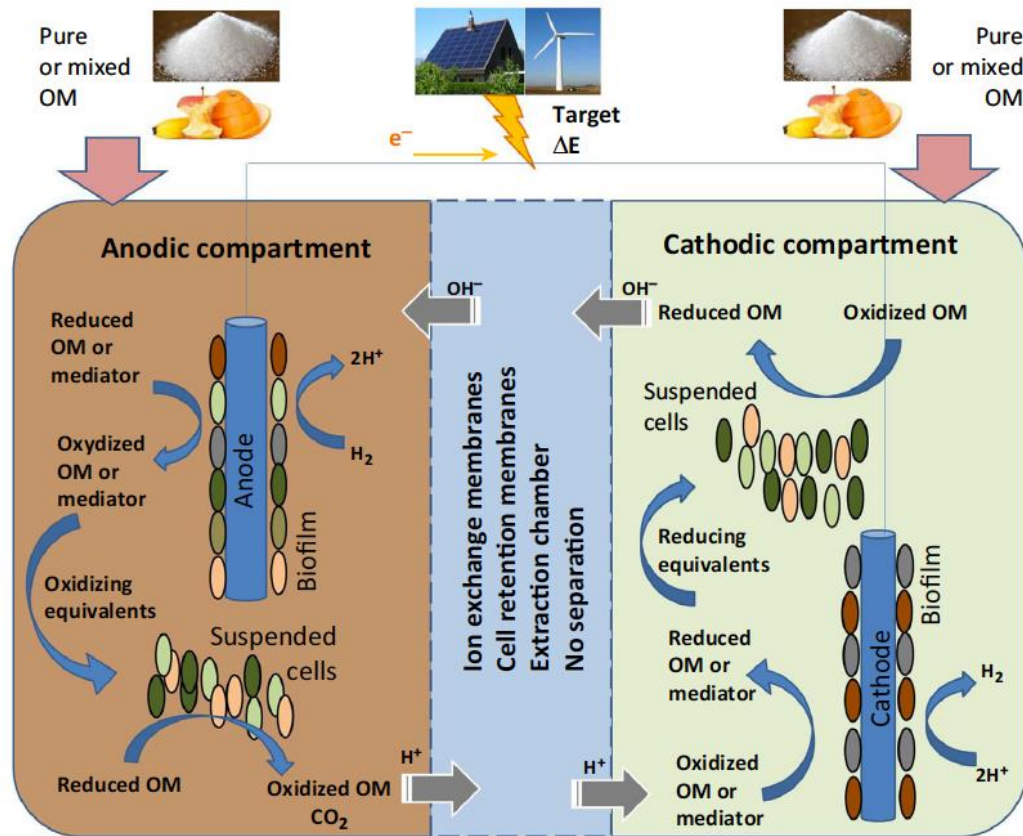
Genus Archaea



Genus Bacterias



ANODE AND CATHODE REACTION IN BES

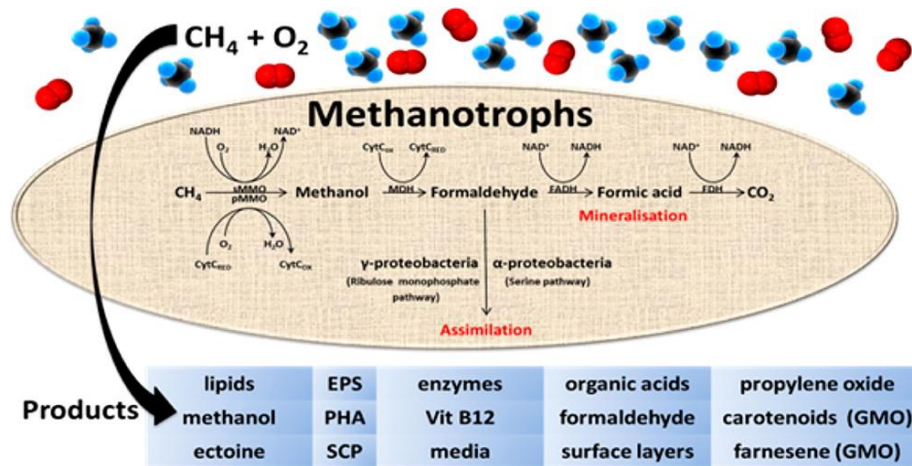
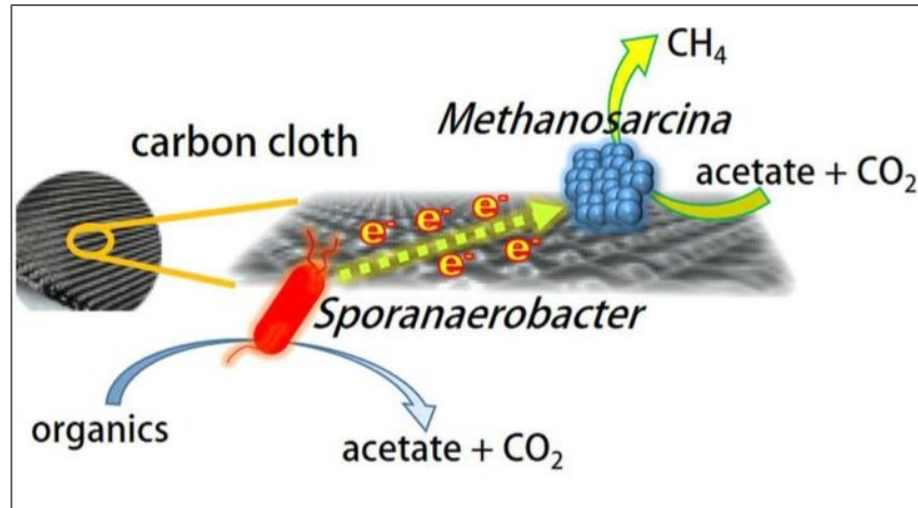


Choi & Sang Biotechnol Biofuels (2016) 9:11

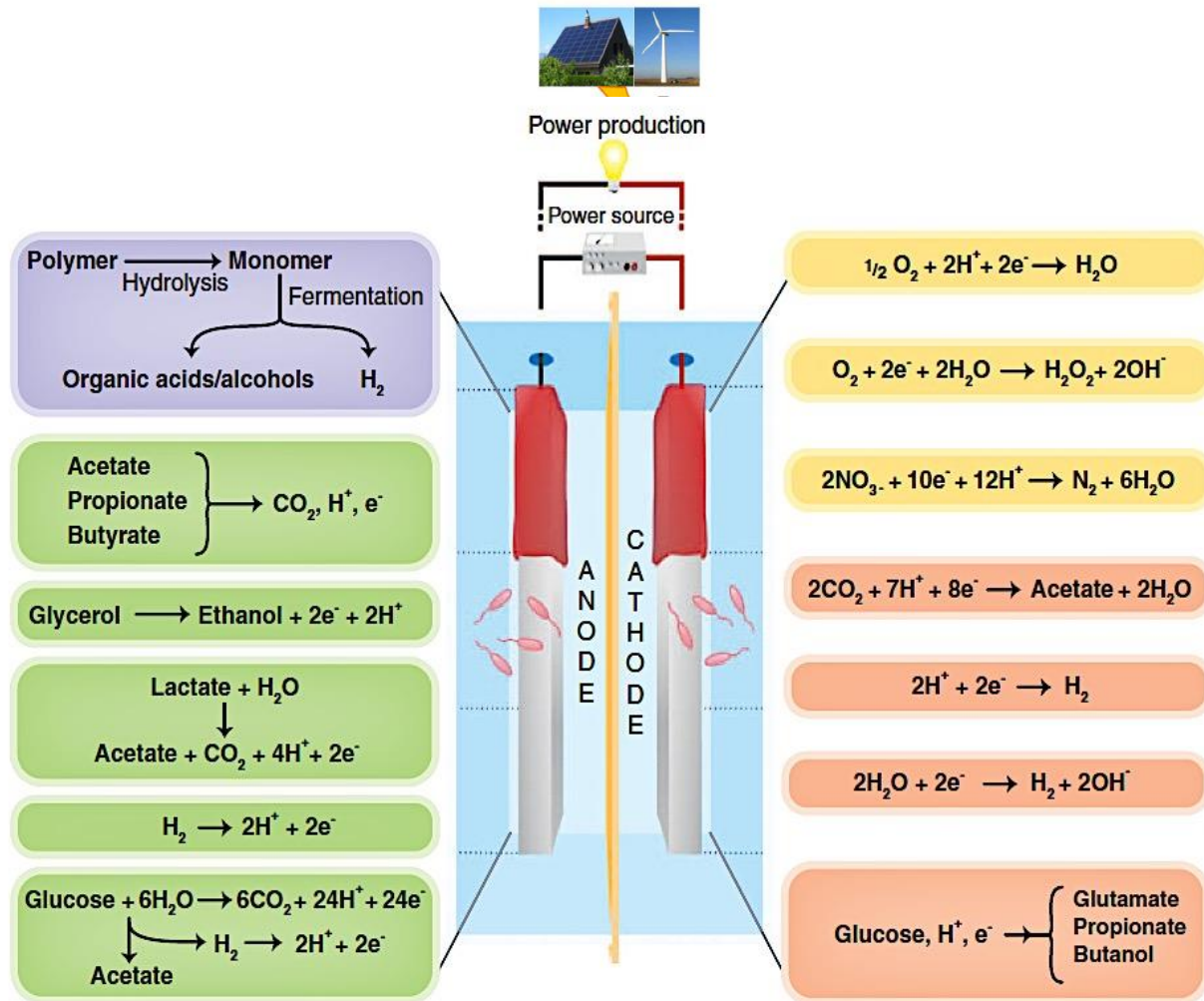
Schievano et al (2016) TIBTEC 1379

Trends in Biotechnology

ELECTROACTIVE MICROORGANISMS AND ELECTROTROPHS



ANODE AND CATHODE REACTION IN BES



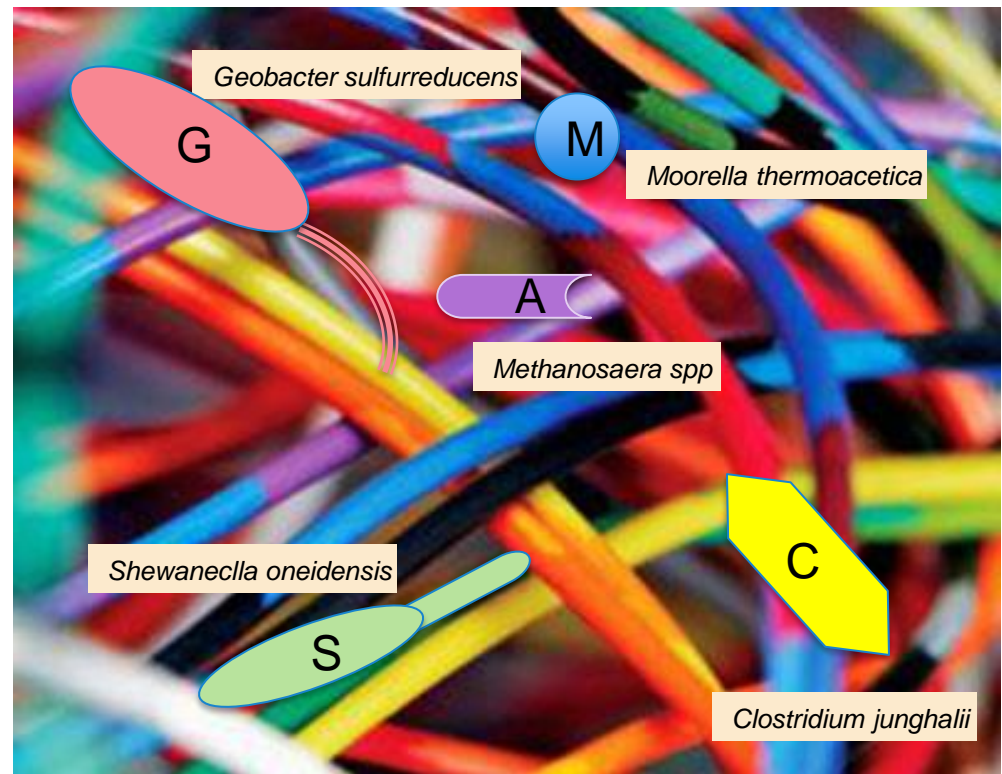
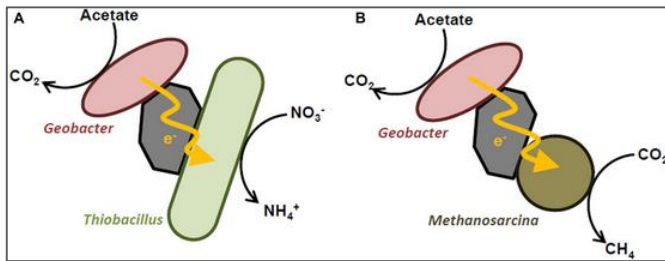
ELECTRON TRANSFER INTER-SPECIES BACTERIA:ARCHAEA

LETTER

doi:10.1038/nature15733

Intercellular wiring enables electron transfer between methanotrophic archaea and bacteria

Gunter Wegener^{1,2*}, Viola Krukenberg^{1*}, Dietmar Riedel³, Halina E. Tegetmeyer^{4,5} & Antje Boetius^{1,2,4}



BCM	Sustrato Anolito	Área y Material Ánodo	Área Cátodo CF	Modificación Cátodo	Dist Elect	Separador	PCA V	Resist Interna Ω	DC Max mA cm⁻²	DP Max mW cm⁻²
Pecera 1	Sedimento sitio 1	CF 0.0112 m ²	0.01125 m ²	Sin Modificación	0.05 m	Barro y Sedimento	0.3	2042	7x10 ⁻⁴	1.2x10 ⁻⁴
Pecera 2	Sedimento sitio 1	CF 0.0112 m ²	0.01125 m ²	Acetato cámara anódica	0.05 m	Barro y Sedimento	0.6	3149	4.8x10 ⁻⁴	7.21x10 ⁻⁵
2a	Sedimento sitio 1	CF 0.00785 m ²	0.00785 m ²	Sin Modificación	0.04 m	Sedimento	0.3	1013	1.5x10 ⁻³	3.1x10 ⁻⁴
3c 1s	Sedimento sitio 1	1 CF Seg 0.00785 m ²	0.00785 m ²	Sin Modificación	0.005 m	Barro	0.48	4592	3.74x10 ⁻⁴	7.48x10 ⁻⁵
3c 2s	Sedimento sitio 1	2 CF Seg 0.00785 m ²	0.00785 m ²	Sin Modificación	0.005 m	Barro	0.77	9847	3.6x10 ⁻⁴	1.6x10 ⁻⁴
3c 3s	Sedimento sitio 1	3 CF Seg 0.00785 m ²	0.00785 m ²	Sin Modificación	0.005 m	Barro	0.58	4613	8.4x10 ⁻⁴	2.52x10 ⁻⁴
3c 4s	Sedimento sitio 1	4 CF Seg 0.00785 m ²	0.00785 m ²	Sin Modificación	0.005 m	Barro	0.67	1195	1.5x10 ⁻³	6.8x10 ⁻⁴
3c 4s Aire en Catolito	Sedimento sitio 1	4 CF Seg 0.00785 m ²	0.00785 m ²	Sin Modificación	0.005 m	Barro	0.33	1314	1.8x10 ⁻³	2.5x10 ⁻⁴

DATA OF DIFFERENT BES CHARACTERIZED

BCM	Sustrato Anolito	Área y Material Ánodo	Área Cátodo CF	Modificación Cátodo	Dist Elect	Separador	PCA V	Resist Interna Ω	DC Max mA cm ⁻²	DP Max mW cm ⁻²
Celda A	Sedimento sitio 4	5 CP Seg 0.0025 m ²	0.00785 m ²	Sin Modificación	0.04 m	Sedimento	0.69	7856	2.2x10 ⁻³	6.5x10 ⁻⁴
Celda B	Sedimento + 3 g. Diésel	4 CF Seg 0.0025 m ²	0.00785 m ²	Sin Modificación	0.04 m	Sedimento	0.6	9371	1.3x10 ⁻³	6x10 ⁻⁴
Celda C	Sedimento + 9 g. Diésel	4 CF Seg 0.0025 m ²	0.00785 m ²	Sin Modificación	0.04 m	Sedimento	0.64	7927	2.7x10 ⁻³	8.7x10 ⁻⁴
Celda D	Sedimento + 15 g. Diésel	4 CF Seg 0.0025 m ²	0.00785 m ²	Sin Modificación	0.04 m	Sedimento	0.56	7199	1.4x10 ⁻³	8.5x10 ⁻⁴
Celda A	Sedimento sitio 4	5 CP Seg 0.0025 m ²	0.00785 m ²	Catalizado KMnO ₄	0.04 m	Sedimento	0.71	1654	4.7x10 ⁻³	1.8x10 ⁻³
Celda B	Sedimento + 3 g. Diésel	4 CF Seg 0.0025 m ²	0.00785 m ²	Catalizado KMnO ₄	0.04 m	Sedimento	0.77	1365	7.2x10 ⁻³	2.3x10 ⁻³
Celda C	Sedimento + 9 g. Diésel	4 CF Seg 0.0025 m ²	0.00785 m ²	Catalizado KMnO ₄	0.04 m	Sedimento	0.76	4162	3.3x10 ⁻³	1.3x10 ⁻³

REFERENCIA	DP Max
Bioresurce Technology (Chandrasekhar et al., 2012)	4.23x10 ⁻⁴ mW cm ⁻² . Lodos de refinera.
Chemical Engineering Journal(Morros et al., 2008)	3.2x10 ⁻³ mW cm ⁻² . Agua subterranea contaminada+diésel. Identificación de bacterias.
Biosensors and Bioelectronics (Li et al., 2016)	1.73x10 ⁻³ mW cm ⁻² . Suelo contaminado con hidrocarburo.Plataforma petrolera

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CALCULO DE PARÁMETROS ELECTROQUÍMICOS

Tiempo de estabilización
25-33 días

$$i = \frac{V}{R}$$

Donde

i= corriente (A)

V= voltaje (V)

R= resistencia (Ω)

$$DC = \frac{i}{S}$$

Donde

i= corriente (mA)

S= superficie (cm²)

DC= densidad de corriente (mA/cm²)

$$DP = \frac{i * V}{S}$$

Donde

i= corriente (mA)

V=voltaje (V)

S= superficie (cm²)

DP= densidad de potencia (mW/cm²)