

# Potential of Small scale Biorefineries in tropical countries

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Small-scale integrated Biorefineries for Rural Development  
in Latin America and Europe Workshop



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# Outline

- Context- Introduction
- Definition of scale
- Biorefinery based on plantain
  - Plantain Pseudostem Biorefinery
  - Plantain Peel Biorefinery
- Definition of scale. A more technical approach
  - Cocoyam
  - Andes Berry
- Conclusions

# Context

1) Fossil-based economies



Bio-economies



Taken from: [goo.gl/4cy5Yh](http://goo.gl/4cy5Yh)



Taken from: [goo.gl/huUYvt](http://goo.gl/huUYvt)

2) "Promoters" for the establishment of bio-economies (De Jong et al., 2012):

Dependence on fossil fuels

Reduction of green-house gases emissions

Boosting regional/rural development

More intensive use/exploitation of raw materials

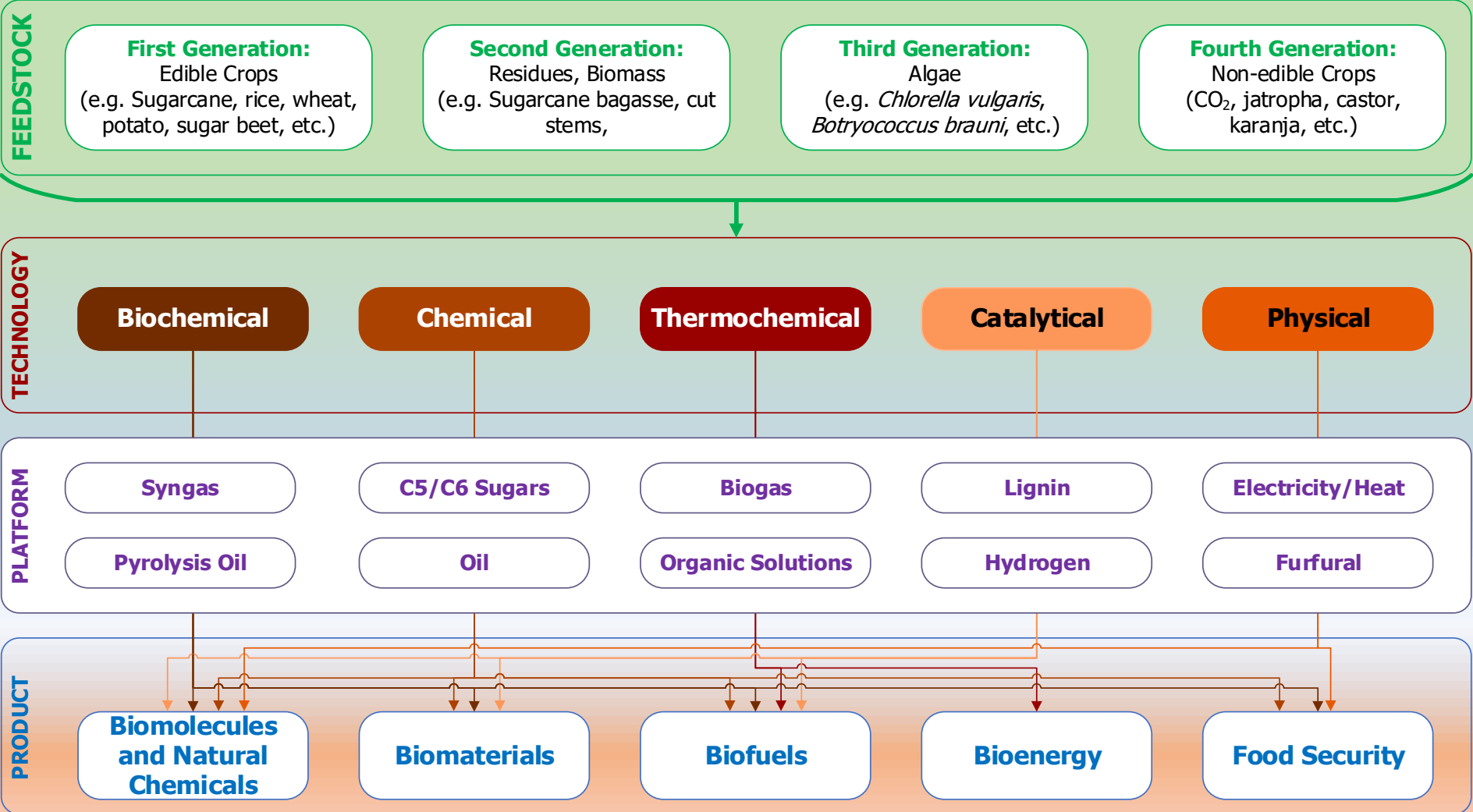


# The Biorefinery Concept.

- The biorefinery concept is analogous to that of oil refinery, fractionating biomass into a family of products including biofuels and bioenergy, biomolecules and natural chemical products, biomaterials and food products that preserve food security. All this as a result of a very deep and comprehensive design to avoid what happened with the oil refineries in the past (Dermibas 2009, Cardona 2011, 2017).



# Context



# Context

Looking for potential biorefineries = Sustainable Biorefineries.

Many questions appear....

## First Level: Feedstocks

A modern biorefinery must integrate first, second and third generation (even 4th) feedstocks with products in order to ensure sustainability.

- What is the best distribution?.
- What is the Economic, Environmental, Social Impact? i.e. Can sustainability be reached
- TAKE DECISIONS, EVALUATE AND ANALYZE.



## Context

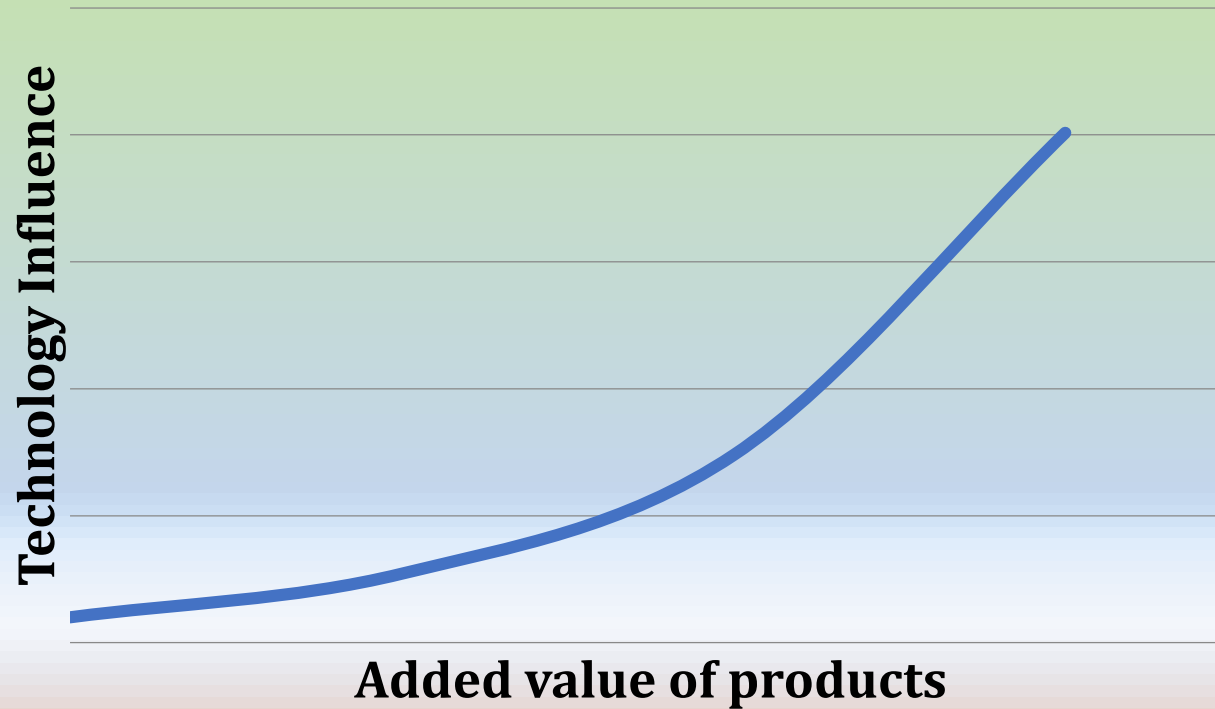
# Sustainable Biorefineries.

- Include objectives for analysis or optimization, evaluating and analyzing impacts:
- **Environmental:** Liquid, Solid, Gas Emissions. Using tools like WAR Algorithm, Life Cycle Analysis, GHG and Carbon Balance.
- **Economical:** Rentability of process, feedstocks charges including Logistics, Locations, Supply Chain, Disponibility of raw materials, Operating Charges among others.
- **Technical:** Evaluation of Productivity, Mass and heat balance.
- **Social:** Employment generation capacity at agronomical, industrial and distribution phase.



# Context

## Biorefineries. Second Level: Technologies.



Generally the influence of technology depends on the added value of products. For this it is important to include a term that emphasize the influence of different stages of production in order to include integrated analysis of technologies.





## Context

# Sustainable Biorefineries.

- Process Integration Strategies.
- Level of Integration. Generation of Different Scenarios using mass, heat, separation-reaction, reaction-reaction integration.



## Sustainable Biorefineries. Third Level: Food Security.

Is it feasible to ensure food security through biorefineries?

Aspects to take into account for food security implications.

- Energy Consumption.
- Land use
- High production cost due to source transportation and quality.
- Use of conventional technology that don't follow the green principles.
- The impact of biorefineries employment on the quality of life



# Context

Biorefineries are designed under specific conditions:

- The typical location for the production of feedstocks is in rural regions and the processing location in other regions with adequate infrastructure in urban zones (Black et al., 2016)

Since the processing facilities have different capacities of production, the operating and capital costs depend on the capacity of the plants.



# Context

Processing facilities are established mainly in two schemes (Palmeros Parada et al., 2017; Santibañez-Aguilar et al., 2015):

## Secondary processing facilities

- > Typically small facilities to reduce transportation costs

## Centralized processing industries

- > Typically large scales to take advantage of the economies of scale



# Context

Economic performance

Production cost

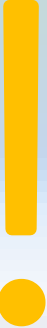
Strong dependence  
on the scale

Energy consumption and equipment cost increase at different rates compared to production scale



# Context

This context shows the importance of a comprehensive analysis of the scale, given the inherent features that will determine the economic performance of a biorefinery if it is operated at a small or a large scale (Kolfshoten et al., 2014)



However, there is not a common definition of large or small scale, or which flow determines a large or a small-scale process.



# Definitions of scale

According to the supply of raw material

*Processing scale:* Amount of raw material processed in a period.

Examples:

A biorefinery that processes raw materials as sugarcane, palm, corn and their respective wastes could be considered as large scale, because the amount of feedstock that is available is very high.



# Definitions of scale

According to the obtainment of product:

*Production scale:* Amount of product obtained in a period.

Examples:

A biorefinery that produces bulk chemicals as ethanol, sugar, butanol, biodiesel could be considered as large scale and one that produces lactic acid, PHB, citric acid could be considered as small/medium scale. However a biorefinery producing antioxidants, flavors, FOS, GOS and antibiotics are mainly small production scale





# Definitions of scale

## Ambiguities in the definitions of scale...

Consider a process to obtain a given metabolite from the peel of a fruit.

- Given the amount of the product in the peel, the production volume will be low because it is a fine or specialty (small scale).
- Given the low concentration of the product in the peel, it is necessary to process a considerable high amount of raw material. In that case, the scale of the process would be higher.

Therefore, it could be argued that the process has two different scales.

The main problem is that the term “scale” is used indistinctly to refer for the amount of raw material or product.(Serna Loaiza et al., 2017)



# Definitions of scale

## Small-Scale Biorefineries

The small-scale biorefineries are the new trend in design because these operations sometimes are unfeasible in large scale due to its production cost or market restrictions in quantity.

Small-scale biorefineries are affected by external factors such as:

- ✓ Government policies.
- ✓ Environmental considerations.
- ✓ Market conditions.
- ✓ Transportation and Distribution costs.

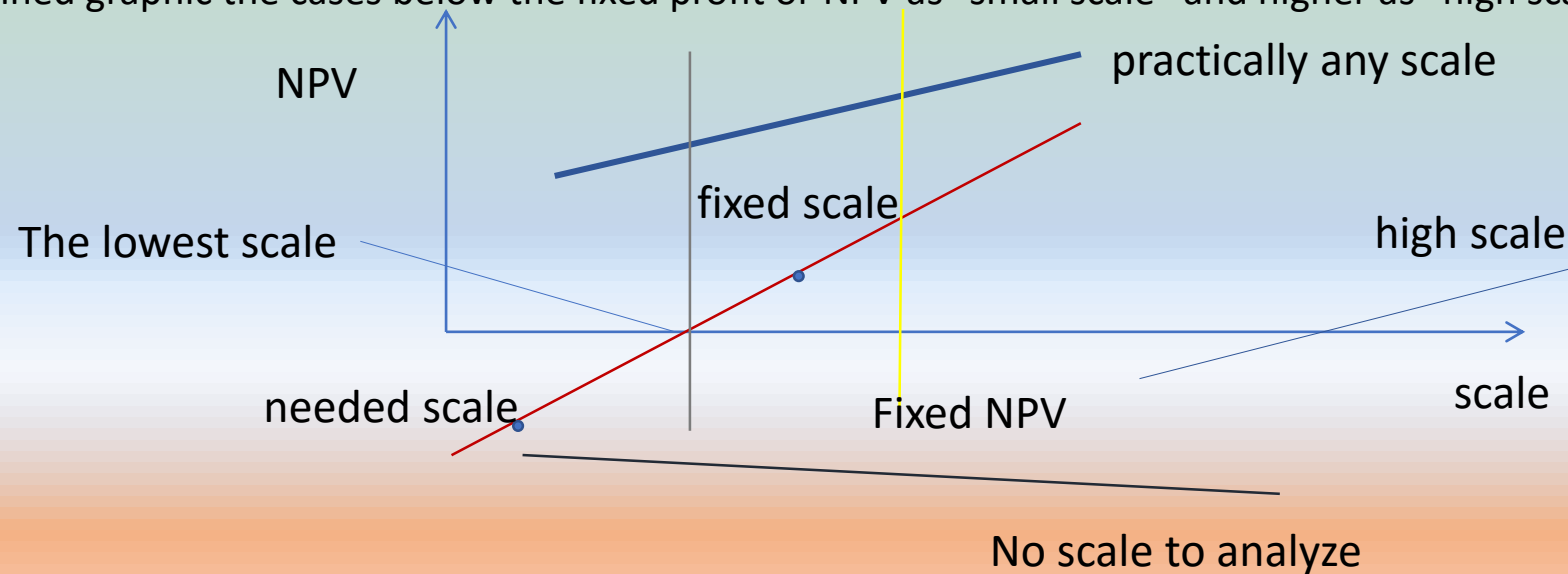


# Definitions of scale

How to define the small or high scale biorefinery. A technical approach.

## Algorithm

1. Calculate your desired biorefinery at any scale.
2. Analyze the production costs, profit and net present value (NPV)
3. Develop the point 2 at different scales and fix the profit or NPV you want.
4. Define in the obtained graphic the cases below the fixed profit or NPV as “small scale” and higher as “high scale”.



# Definitions of scale

How to define the small or high scale biorefinery. A technical approach.

Algorithm (cont)

5. Based on conceptual design, transform the lower profit or NPV for small scale biorefineries as a challenge for your design: How can we make these small scale cases as profitable?:

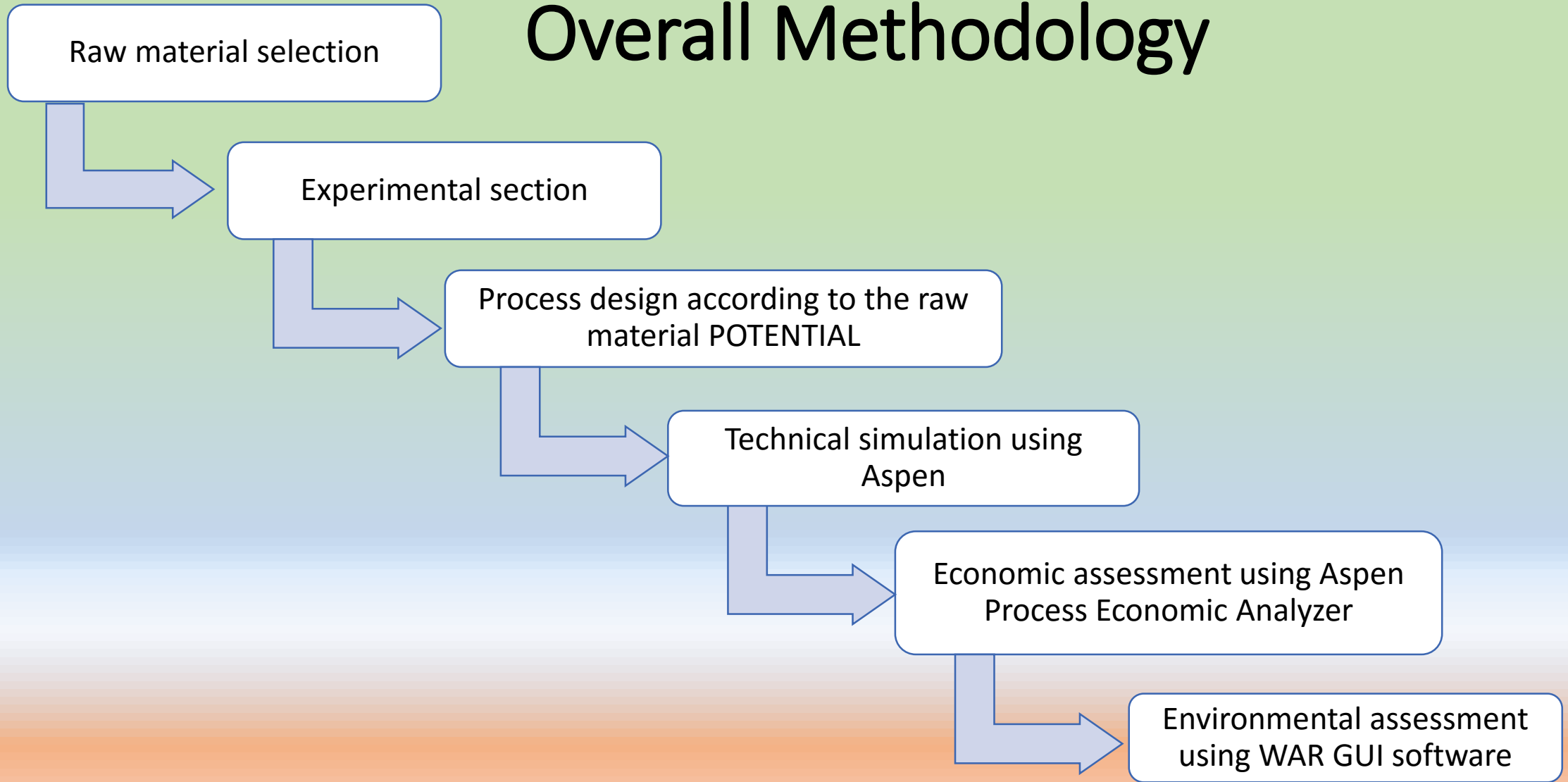
- Integration
- Increase the number or fraction of high value added products
- Technology changes

6. Redefine your problem or target as needed and repeat points 1-4.



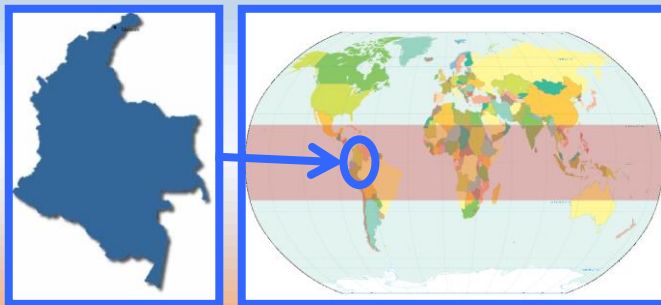
# Definitions of scale

## Overall Methodology



# Some of the thousands of Agricultural Residues in a tropical country as Colombia

Crop	Residue	Residues Generated [ton/year]
Coffee	Coffee Pulp	301.848
	Spent Coffee	257.962
Cocoa	Cocoa Husks	59.756.000
Rice	Rice Husks	562.964
Plantain	<b>Plantain Pseudostem</b>	<b>1.699.137</b>
Cassava	Cassava stem	91.335





# CASE 1. PLANTAIN

## Example 1 Plantain Pseudostem (PP)

The plantain pseudostem is the non-edible part of the plantain plant, it represent the 50 % of total biomass

7.3 million tons of plantain pseudostem was produced in 2014

Plantain Pseudostem is used for nutrient assistance of new plants. But also in the paper fabrication and currently, as raw material for the production of sugars to obtain other added-value products



**Table 1.** Chemical Composition PP

Component	% dry basis
Cellulose	43.46
Hemicellulose	33.77
Lignin	20.14
Extractives	2.5
Ash	0.14

**Figure 2.** Plantain Pseudostem



# CASE 1 PLANTAIN

## Example 2. Plantain Peel



**Figure 3.** Plantain Peel

Represents between 30% and 40% of the total fruit weight

Approximately 1 kilogram of plantain bunches produces 360 grams of plantain peel

**Applications studies**



Starch extraction for the food industry, extraction of phenolic compounds and antioxidants

**Table 2.** Chemical Composition Plantain Peel

Component	% dry basis
Cellulose	27.7
Hemicellulose	22.7
Lignin	27.9
Crude Protein	7.4
Extractives	7.9
Ash	6.4





## 2. PROCESS DESCRIPTION

# Plantain Pseudostem Biorefinery

### Acid Hydrolysis

Sulfuric Acid 2%w/w  
Temperature = 122°C  
Water to Solid Ratio (WSR) = 8g/g

### Detoxification

Overliming with Lime  
Temperature = 60°C

### Alkaline treatment

NaOH 2 %w/v  
Temperature = 120°C  
Water to Solid Ratio = 10 g/g

### Enzymatic Saccharification

Celluclast 1.5L  
Temperature = 45°C  
Biomass to Enzyme Ratio = 2% w/v

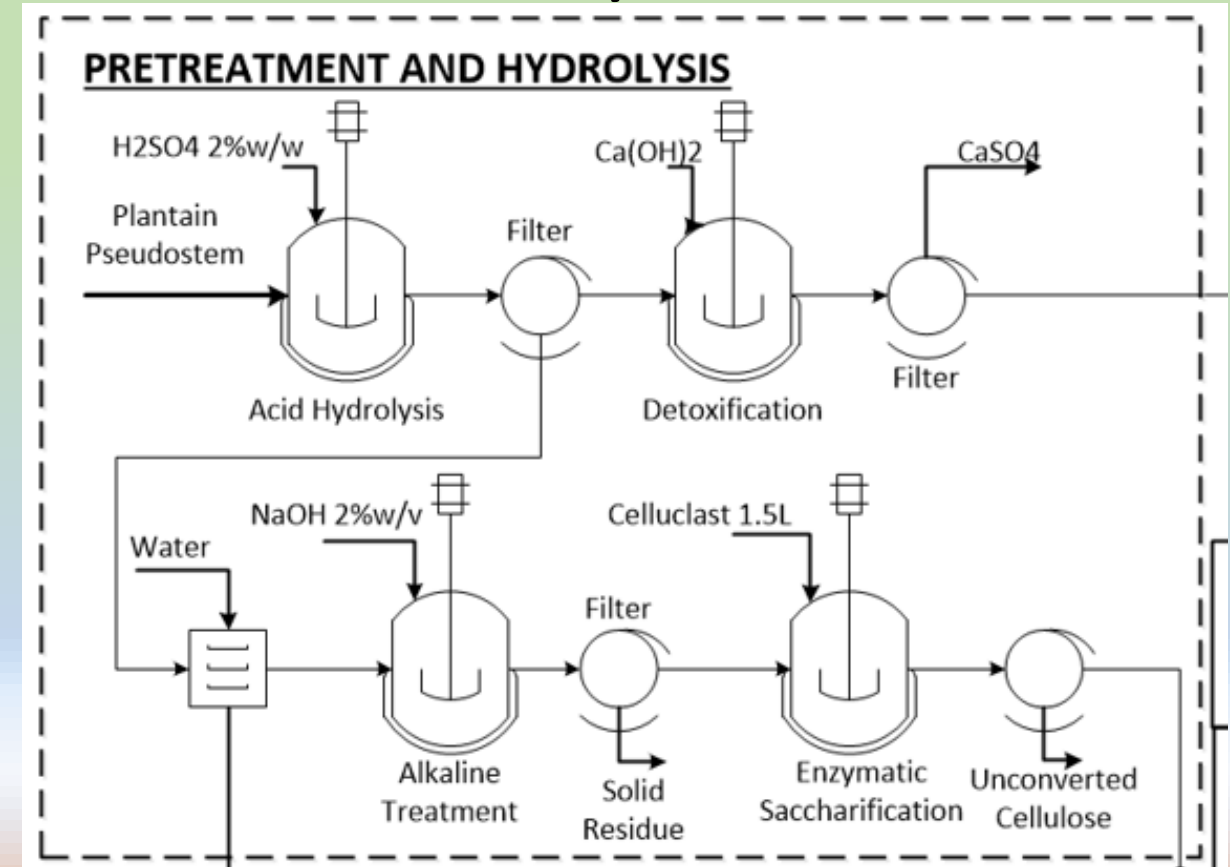


Figure 4. Pretreatment Process Scheme



## 2. PROCESS DESCRIPTION

# Plantain Pseudostem Biorefinery

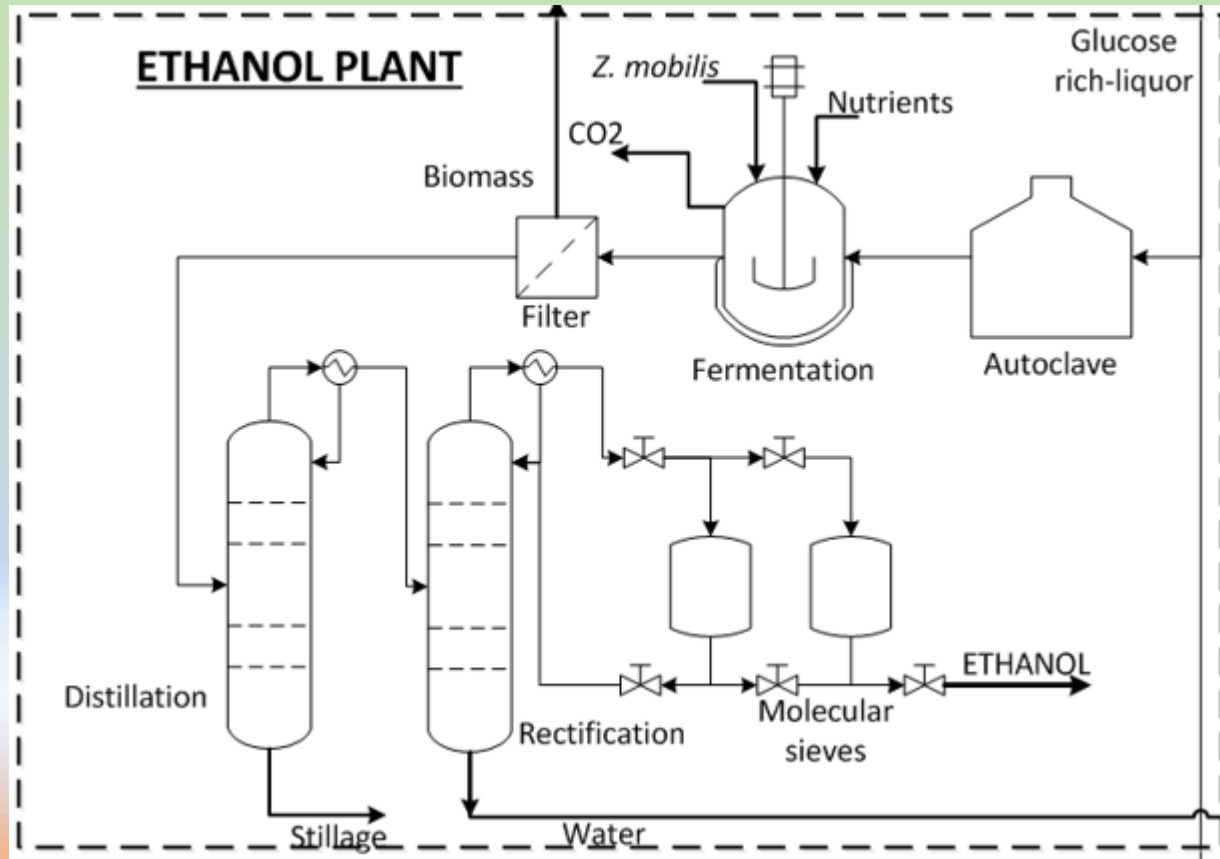


Figure 5. Ethanol Process Scheme

### Fermentation

Microorganism = *Z. mobilis*  
Temperature = 30°C

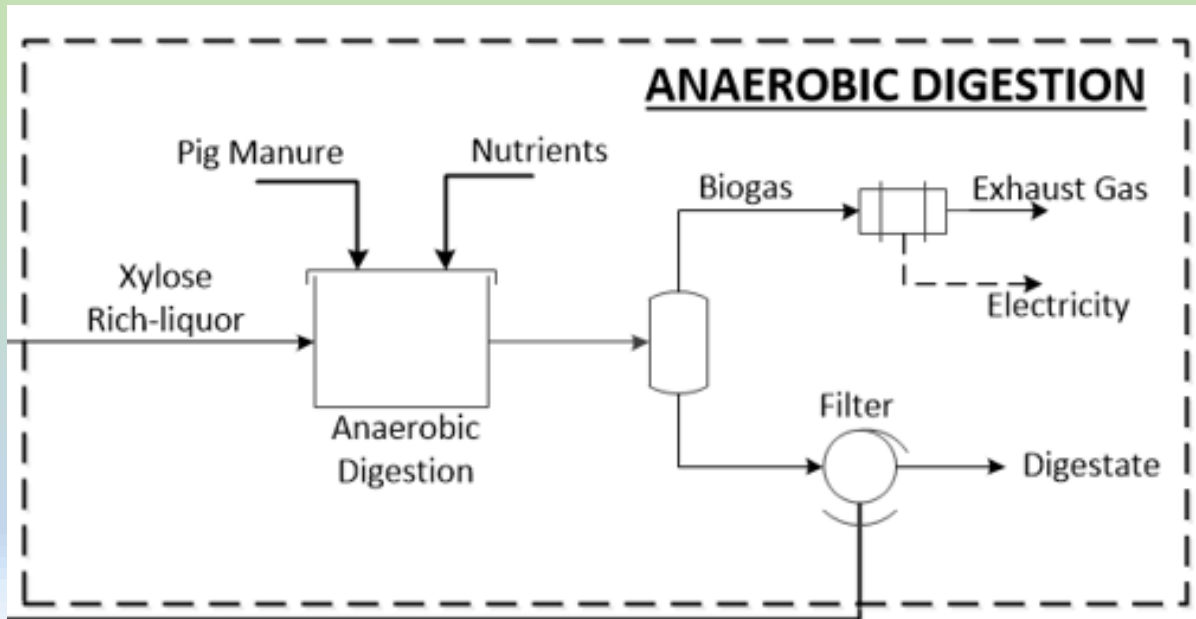
### Downstream

Distillation column = Ethanol 50-55%wt.  
Rectification column = 96%wt.  
Molecular Sieves = 99.7%wt.



## 2. PROCESS DESCRIPTION

# Plantain Pseudostem Biorefinery



**Figure 6.** Anaerobic Digestion Process Scheme

### Anaerobic Digestion

Inoculum = Pig Manure

Substrate to Inoculum Ratio = 1:2

Temperature = 37°C

Electricity generation from biogas = 1.7 kWh/cum biogas



## 2. PROCESS DESCRIPTION

# Plantain Peel Biorefinery

### Acid Hydrolysis

Sulfuric Acid 2%w/w  
Temperature = 122°C  
Water to Solid Ratio (WSR) = 10 g/g

### Detoxification

Overliming with Lime  
Temperature = 60°C

### Alkaline treatment

NaOH 1 %w/v  
Temperature = 121 °C  
Water to Solid Ratio (WSR) = 8 g/g

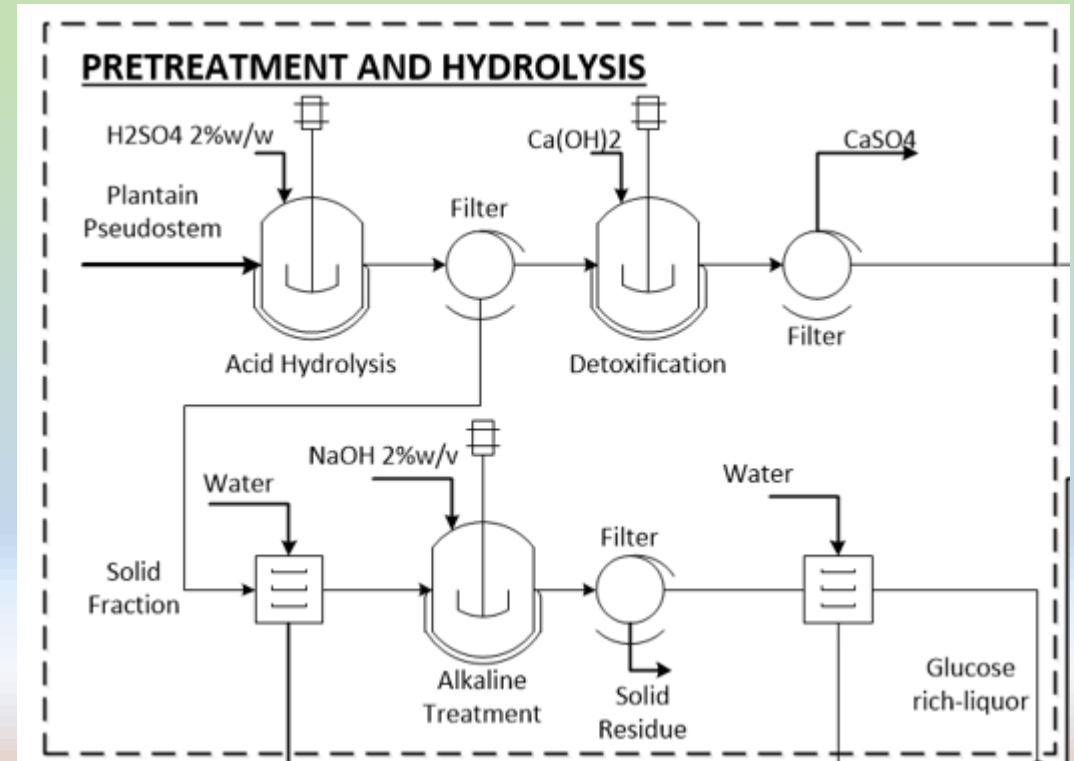
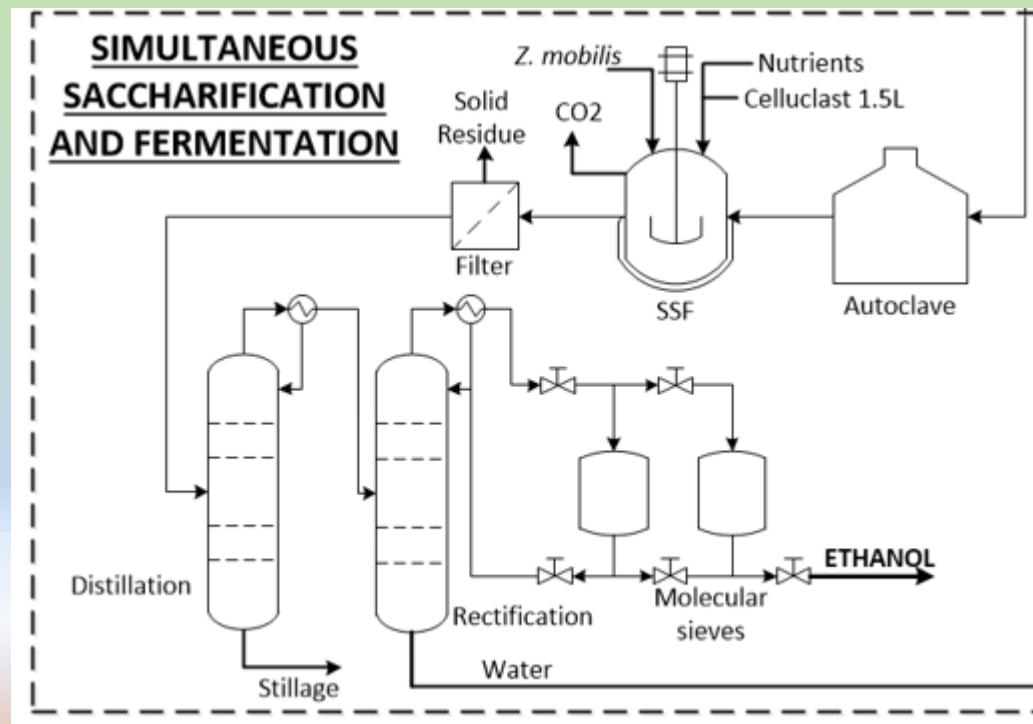


Figure 7. Pretreatment Process Scheme



## 2. PROCESS DESCRIPTION

# Plantain Peel Biorefinery



### Simultaneous saccharification and fermentation

Enzyme = Celluclast 1.5L

Temperature = 40°C

Biomass to Enzyme Ratio = 2% w/v

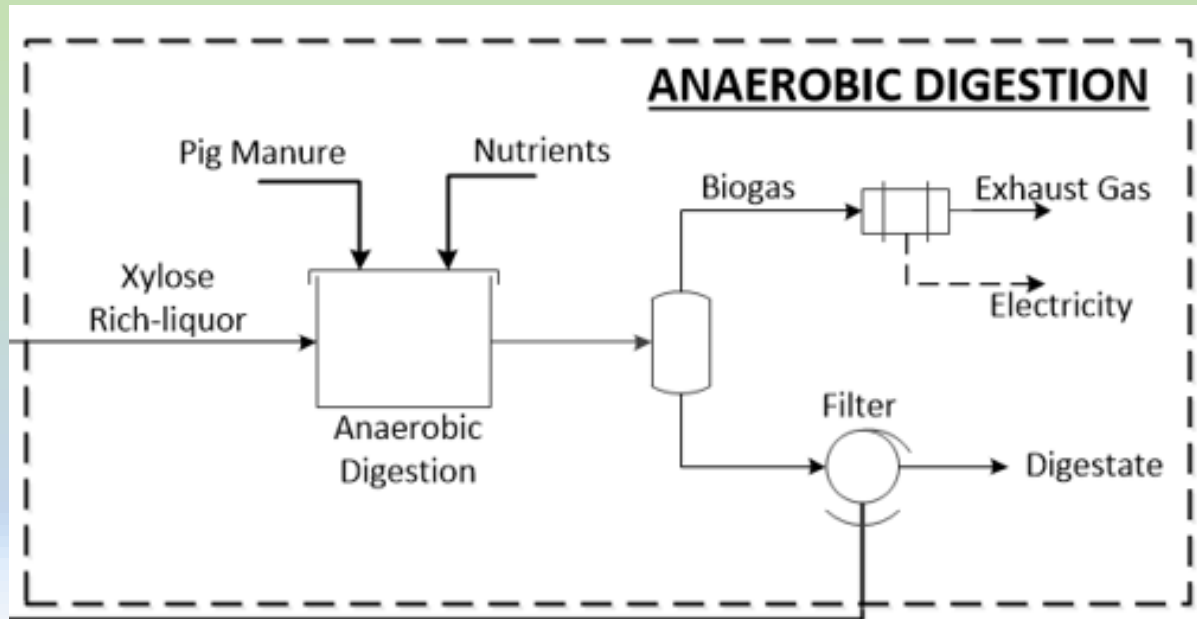
Microorganism (ethanol) = *Saccharomyces Cerevisiae*

**Figure 8.** Simultaneous saccharification and fermentation Process Scheme



## 2. PROCESS DESCRIPTION

# Plantain Peel Biorefinery



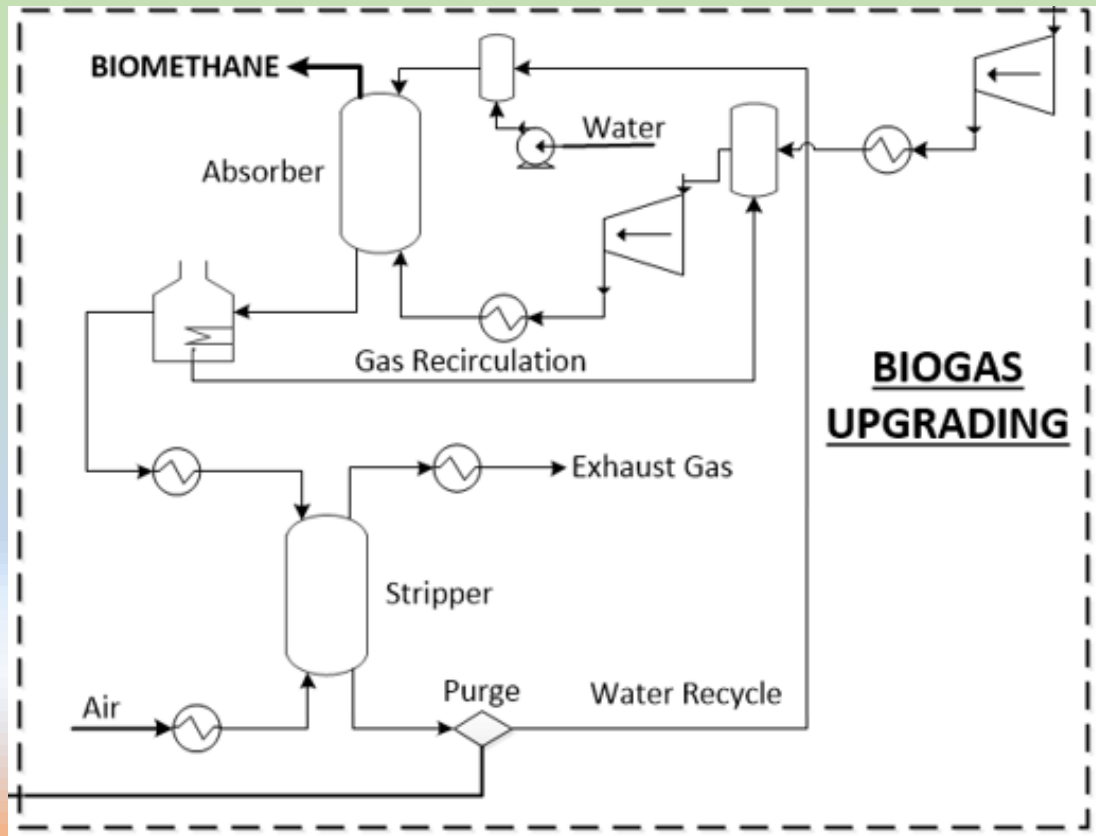
**Figure 9.** Anaerobic Digestion Process Scheme

**Anaerobic Digestion**  
Inoculum = Pig Manure  
Substrate to Inoculum Ratio = 1:2  
Temperature = 37°C  
Electricity generation from biogas = 1.7 kWh/cum biogas



## 2. PROCESS DESCRIPTION

# Plantain Peel Biorefinery



**Figure 10.** Biomethane Process Scheme

### Biogas Upgrading (Absorption and Stripping)

#### *Absorber*

Pressure = 10 bar  
Temperature = 20°C  
Absorption agent = Water

#### *Stripper*

Pressure = 1 bar  
Temperature = 20°C  
Stripping Agent = Air



## 2. PROCESS DESCRIPTION

# Biomass integrated gasification combined cycle (BIGCC)

Biomass dryer, gasification chamber, gas turbine and heat steam recovery generator (HRSG)

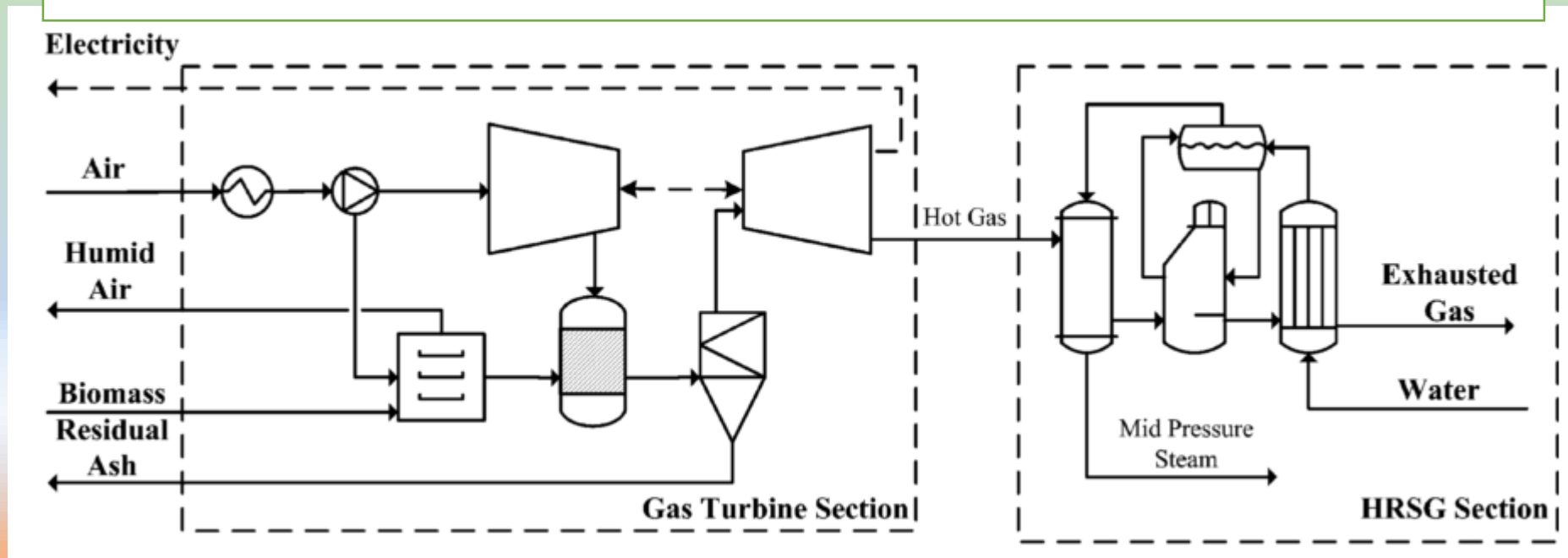


Figure 11. Cogeneration Process Scheme





### 3. RESULTS

## Process Simulation for plantain

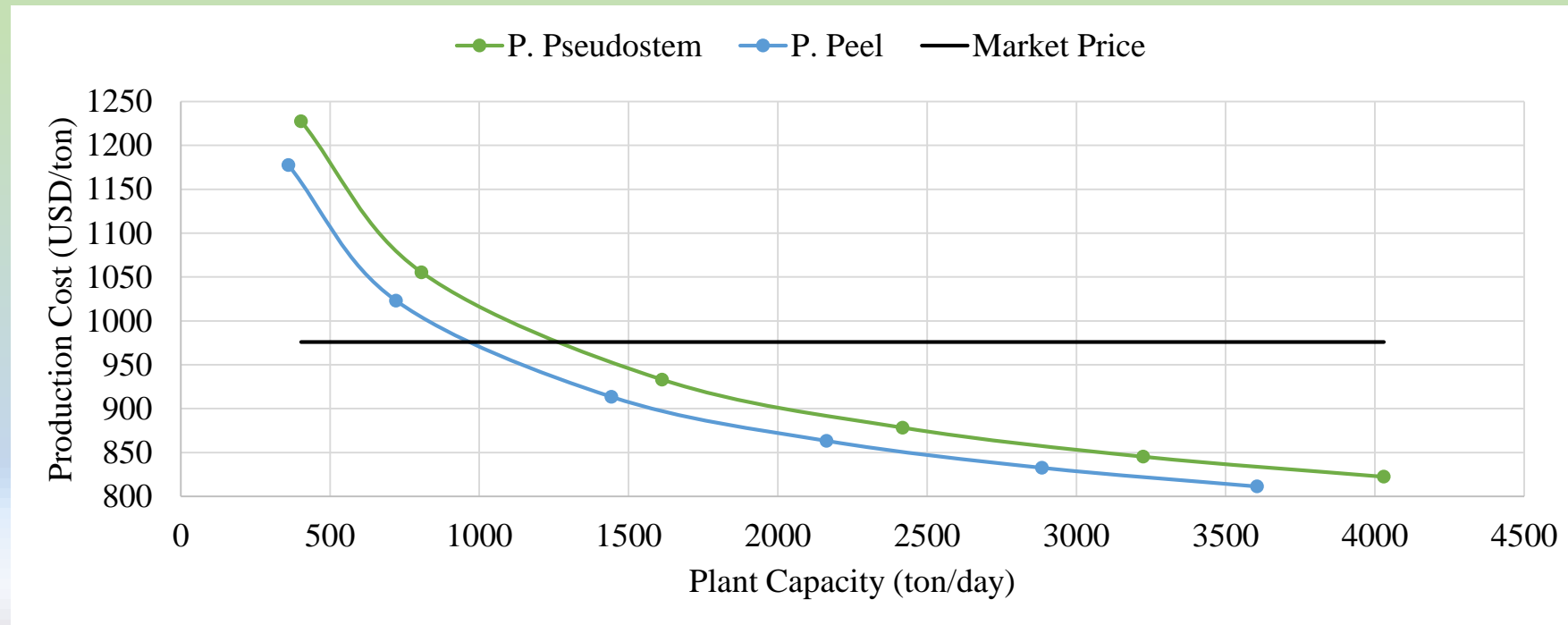
**Table 3.** Bioethanol productivity and yield of the integrated biorefinery

Products	Productivity		Yield	
	Value	Unit	Value	Unit
Plantain Pseudostem	148.31	m <sup>3</sup> /day	102.85	L/ton
Plantain Peel	17.62	m <sup>3</sup> /day	0.29	L/ton



# 3. RESULTS

## Economic Assessment

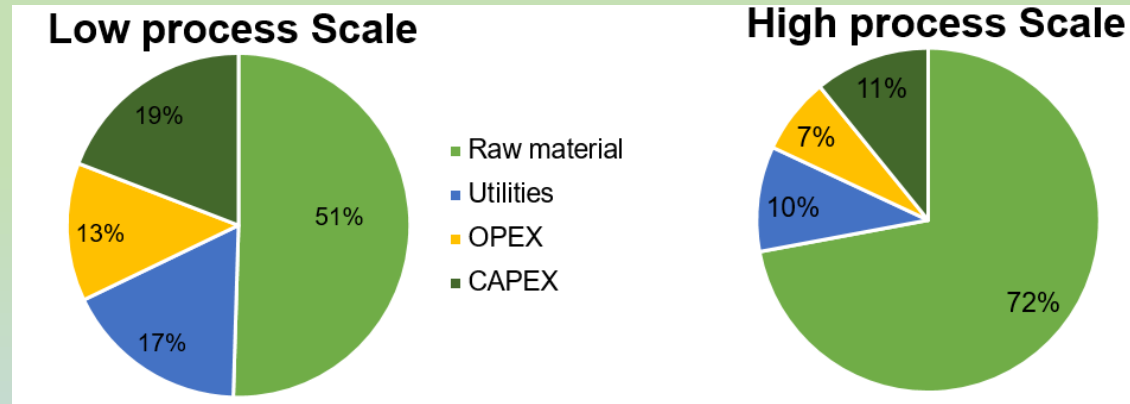


**Figure 12.** Effect of each plant processing capacity in the production cost of the bioethanol.

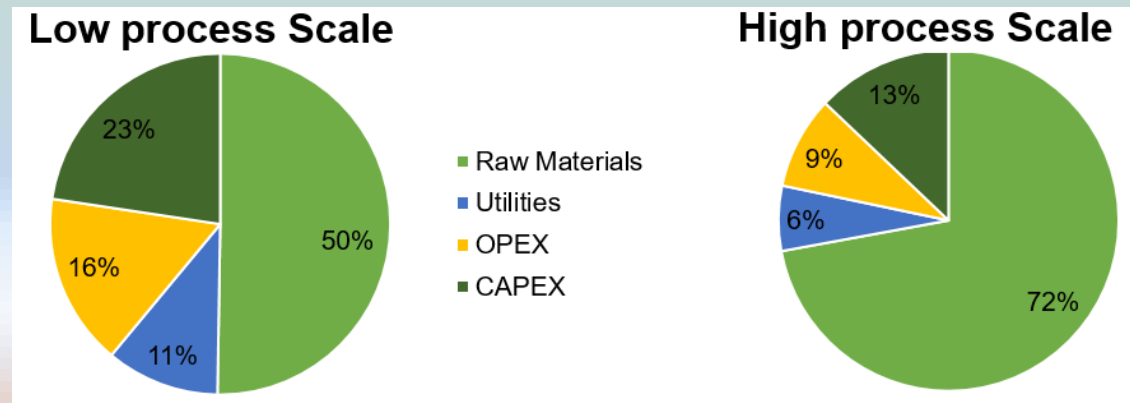


# 3. RESULTS

## Economic Assessment



**Figure 13.** Effect of the process scale in the contribution of the main economic parameters of the pseudostem biorefinery

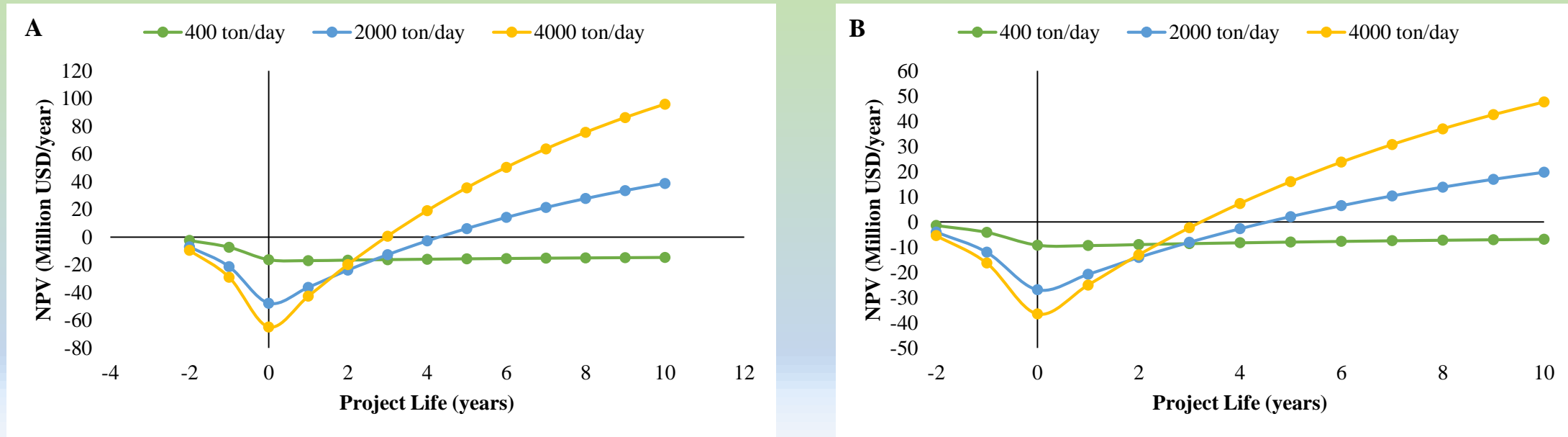


**Figure 14.** Effect of the process scale in the contribution of the main economic parameters of the plantain peel biorefinery



# 3. RESULTS

## Economic Assessment

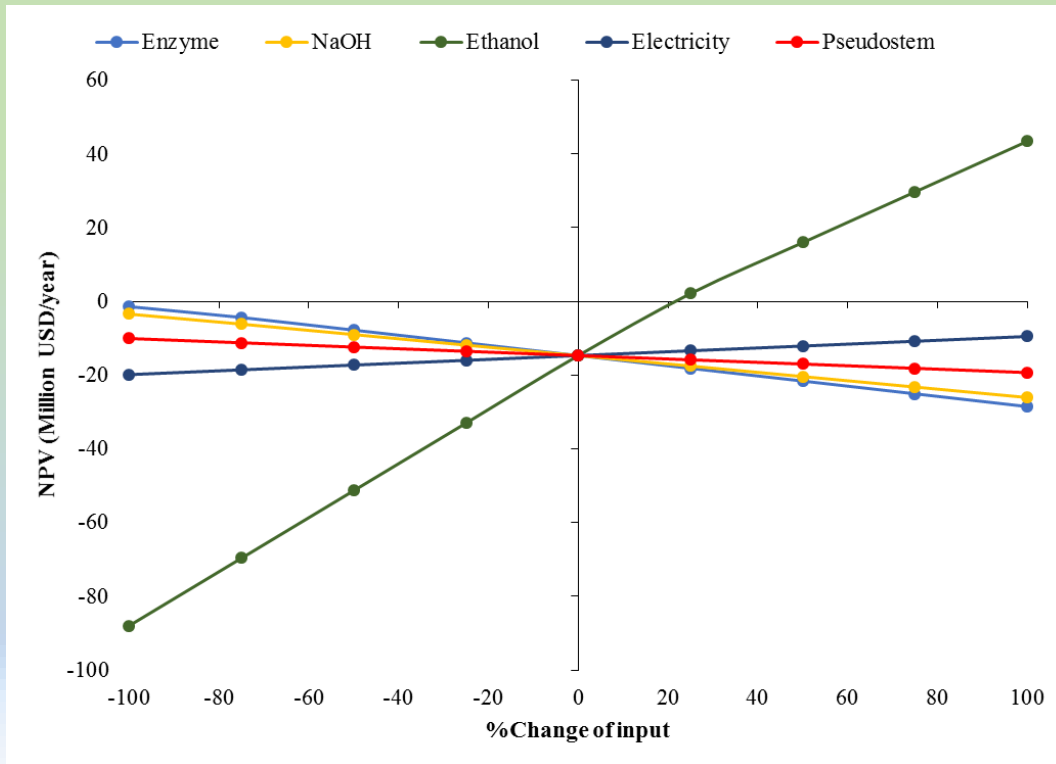


**Figure 15.** Effect of the plant capacity in the economic profitability of the biorefinery. A. Plantain Pseudostem. B. Plantain Peel

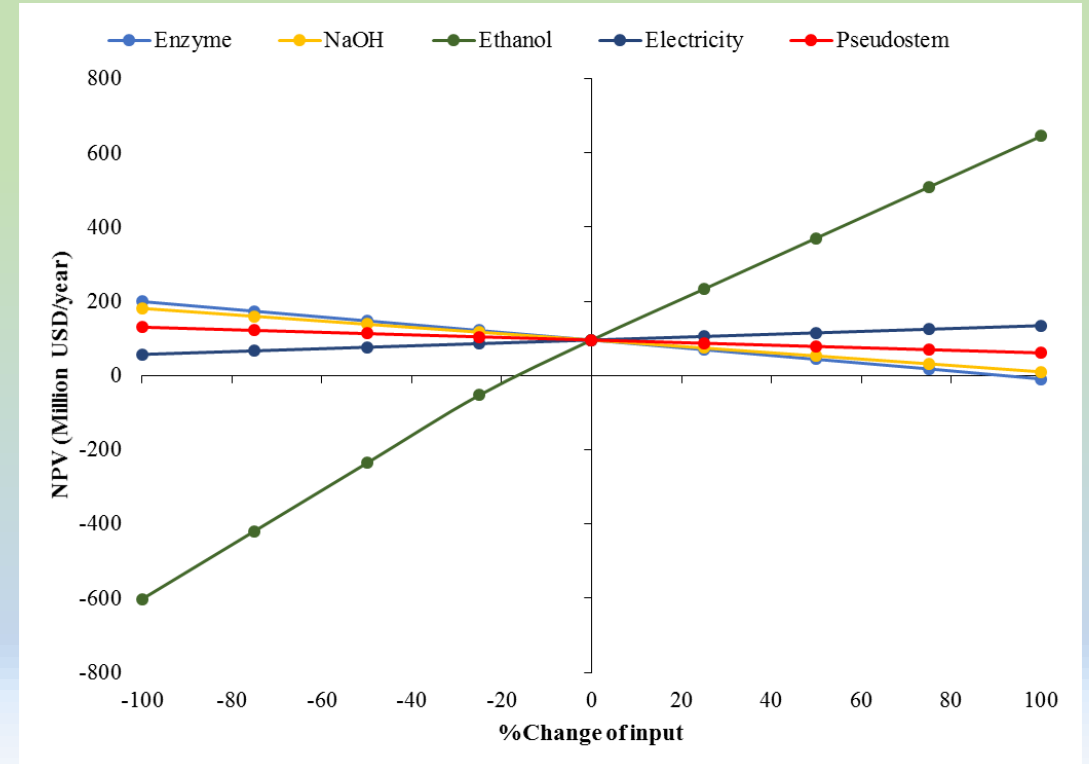


### 3. RESULTS

## Market Price Sensibility Analysis: Pseudostem



**Figure 16.** Market Price Variations of low-scale biorefinery (200 ton/day)

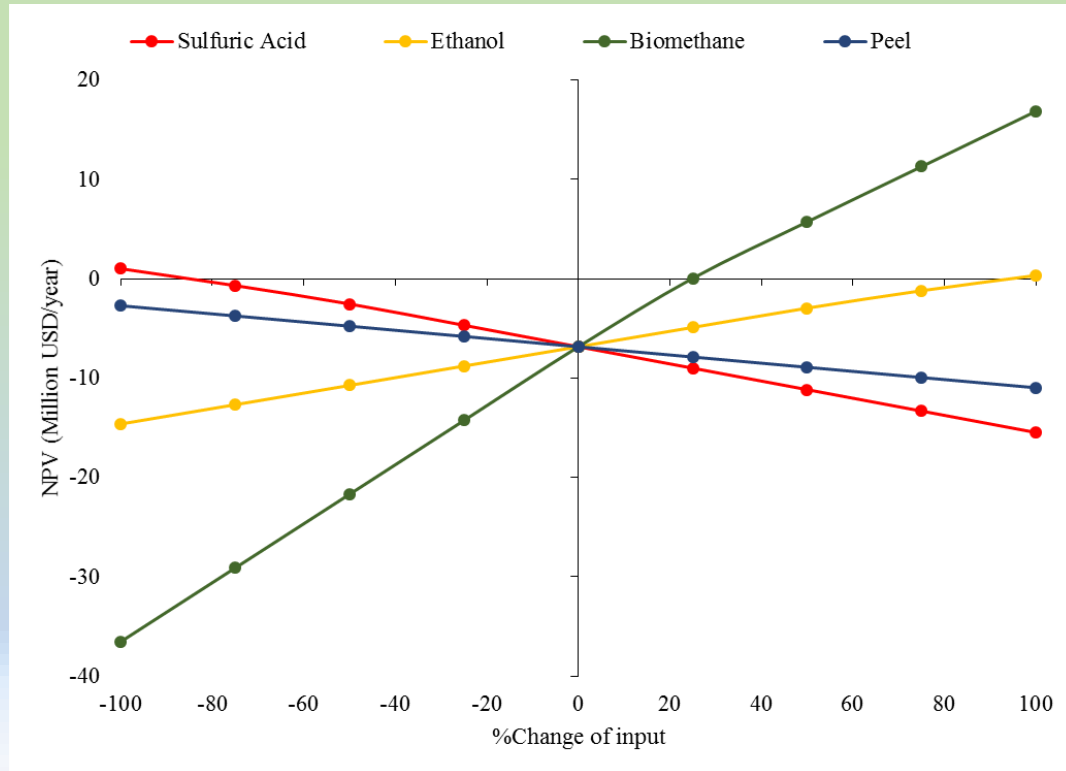


**Figure 17.** Market Price Variations of high-scale biorefinery (2,000 ton/day)

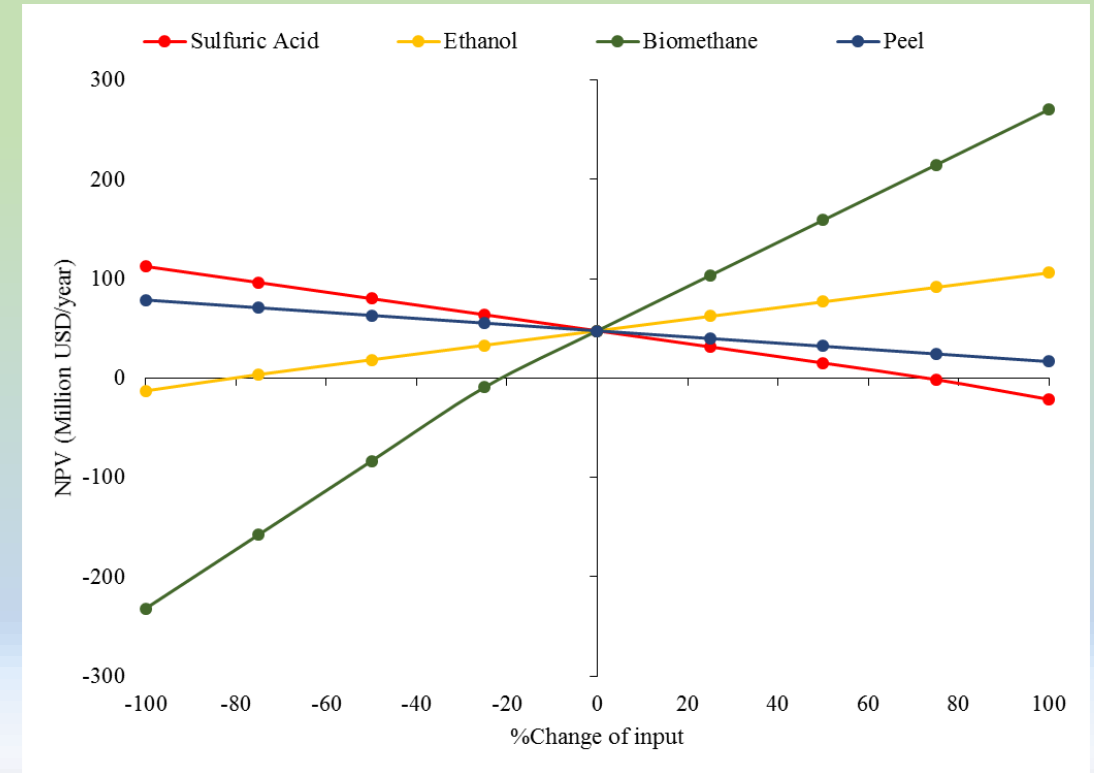


# 3. RESULTS

## Market Price Sensibility Analysis: Peel



**Figure 18.** Market Price Variations of low-scale biorefinery (200 ton/day)

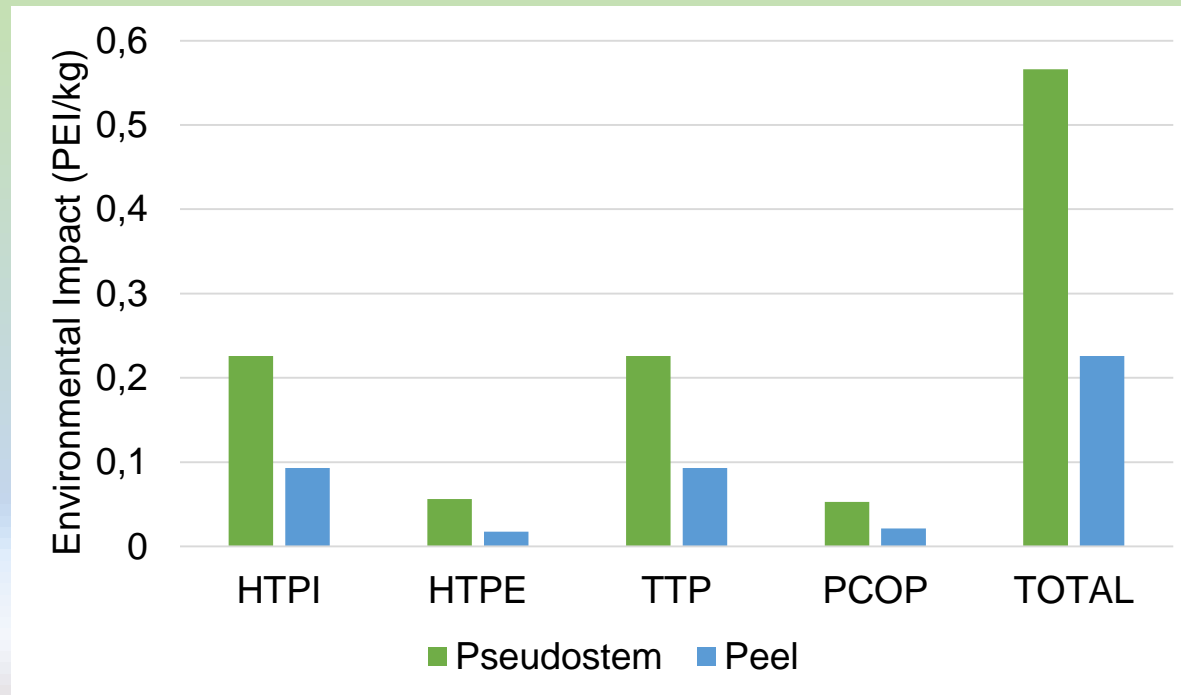


**Figure 19.** Market Price Variations of high-scale biorefinery (2,000 ton/day)



### 3. RESULTS

## Environmental Assessment



**Figure 20.** Potential Environmental Impact of the Integrated Biorefinery

**High Contribution to PEI**  
Human Toxicity by Ingestion (HTPI) and  
Terrestrial Toxicity Potential (TPP)

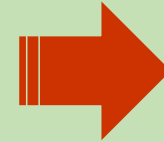


**LD<sub>50</sub> (Lethal Dose)**  
Xylose = 23,000 mg/kg  
Glucose = 25,800 mg/kg



# Definitions of scale to analyze the potential of the biorefinery at different scales....proposing a more technical strategy

Processing scale: Amount of raw material processed in a period.



Ambiguities!

Production scale: Amount of product obtained in a period.

## New definition...

*(Minimum Processing Scale for Economic Feasibility – MPSEF):*

Minimum scale of processing the raw material at which a process achieves a feasible economic performance ( $VPN=0$  during the lifetime of the project). (Cardona, 2015)





# Analysis of Scale

**Objective:** Determining the flow of raw material at which the biorefinery will have a positive economic performance, and determine the minimum feasible small-scale from this point

Processing scale

Vs.

NPV

Variables to determine previous to the analysis of scale

Upper limit

Base case

Lower limit

} Based on the availability, production and specific conditions of the raw material

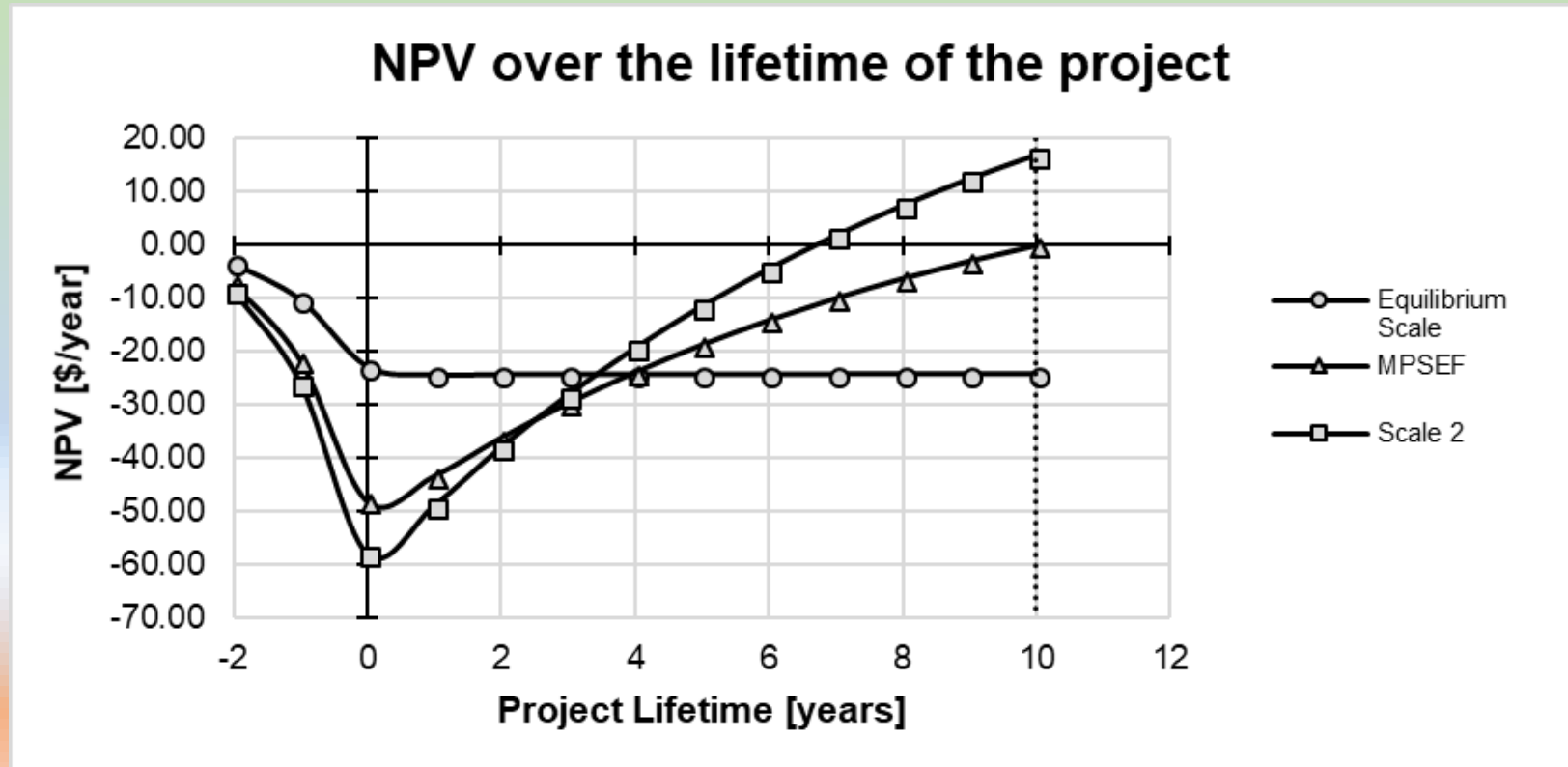


# Analysis of Scale

Processing scale

Vs.

NPV



# Analysis of Scale

Important scales to determine:

*Equilibrium scale:*

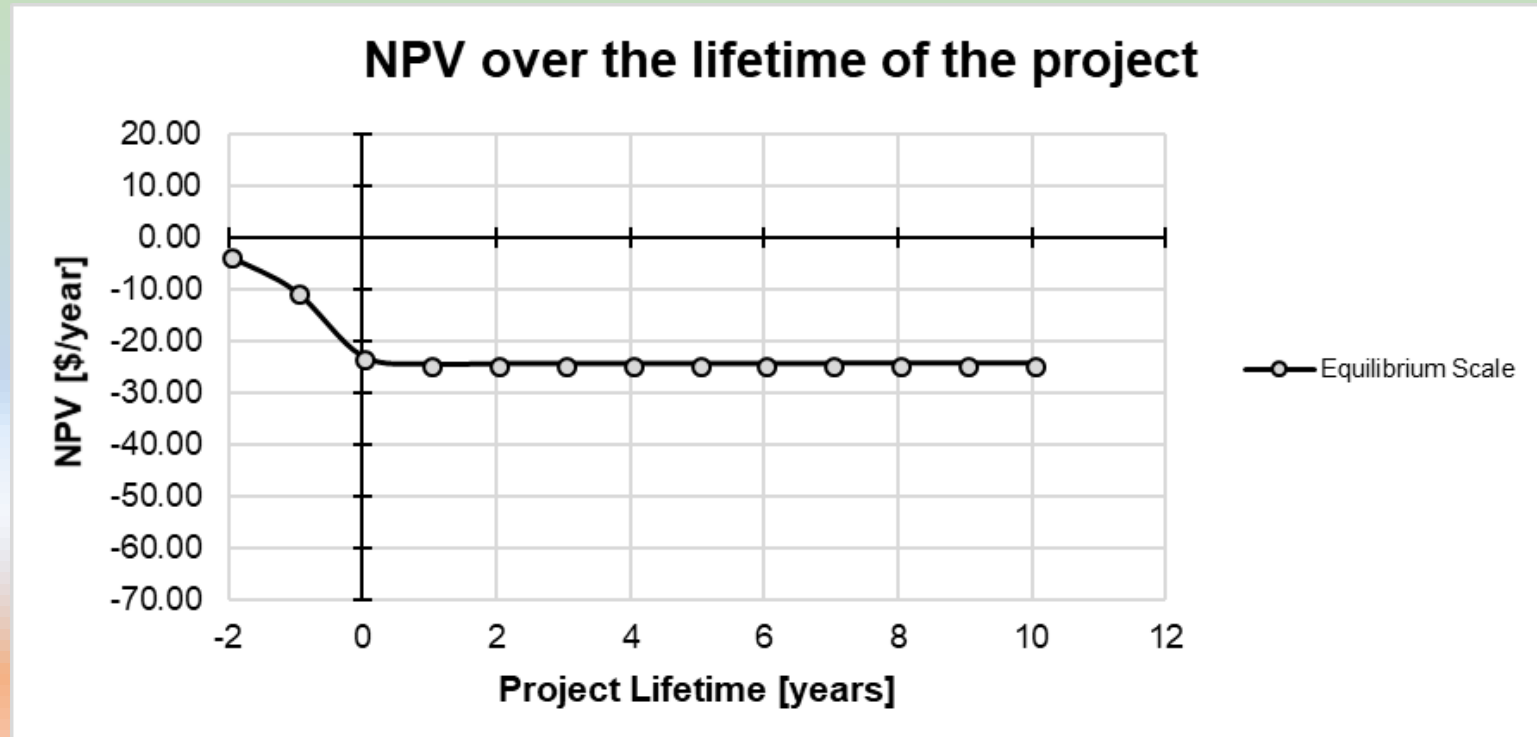
Processing scale at which the relationship between the incomes and the expenses become constant but usually negative. This scale will be named as the Equilibrium Scale and it shows that the process could be feasible only if some external factors provide economic benefits to the process (e.g. governmental subsidies to decrease given taxes or utilities cost) or new configuration of products should be applied



# Analysis of Scale

Important scales to determine:

*Equilibrium scale:*



# Analysis of Scale

Important scales to determine:

*Minimum processing scale for economic feasibility (MPSEF):*

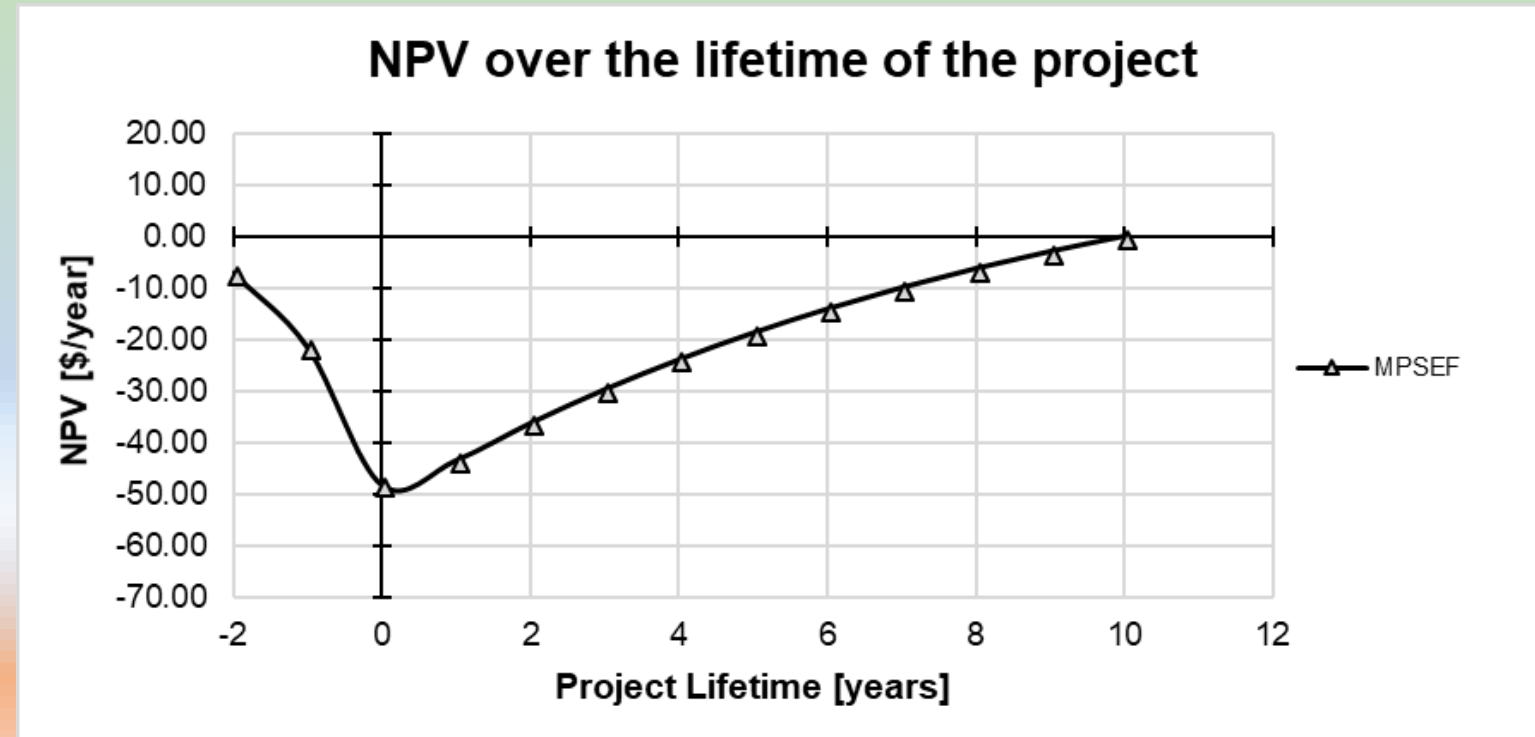
Processing scale at which the process will achieve an accumulated NPV of zero after the total lifetime of the project. This implies that the process will use the entire planned lifetime to recover the investment and no profits will be generated. Every processing scale below the MPSEF will not have a positive economic performance and all those superior to the MPSEF will at least reach positive economic performance and generate profits.



# Analysis of Scale

Important scales to determine:

*MPSEF:*



# Minimum processing scale for economic feasibility

## Examples of application:

### *Cocoyam-based biorefinery:*

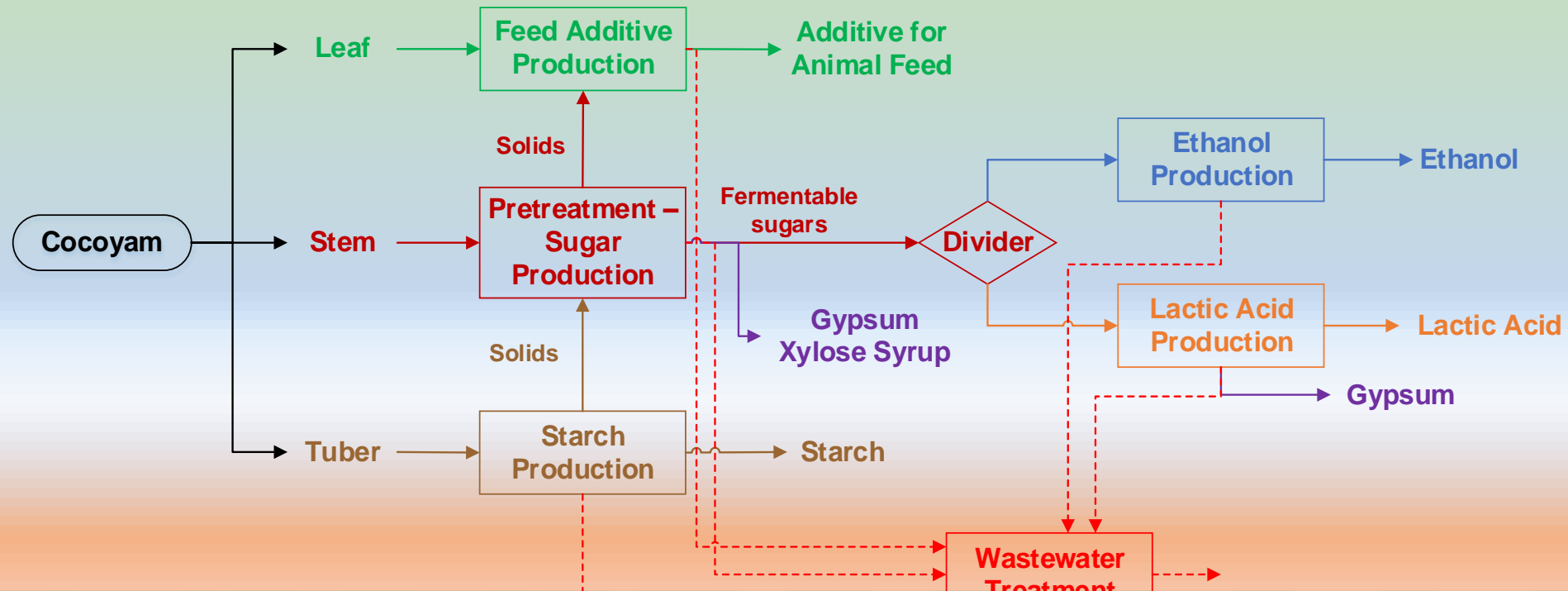
Cocoyam (*Xanthosoma sagittifolium*) is a tropical plant grown in countries of West Africa, Asia and Oceania. This plant belongs to the family of Araceas and grows between 500-2,000 meters above sea level (Giacometti and León, 1992; Gómez and Acero Duarte, 2002). It has been studied due to the different components and platforms that it has on its matrix (protein, lignocellulosics, and starch, among others) and different researches have been done for the production of animal feed, starch, starch-based compounds, beverages, and for biotechnological uses as the production of lactic acid and ethanol (Ndukwu et al., 2017; Owusu-Darko et al., 2014; Régnier et al., 2013; Serna-Loaiza, 2018; Shiraishi et al., 1995).



# Minimum processing scale for economic feasibility

## Examples of application:

*Cocoyam-based biorefinery (Serna-Loaiza, 2017):*



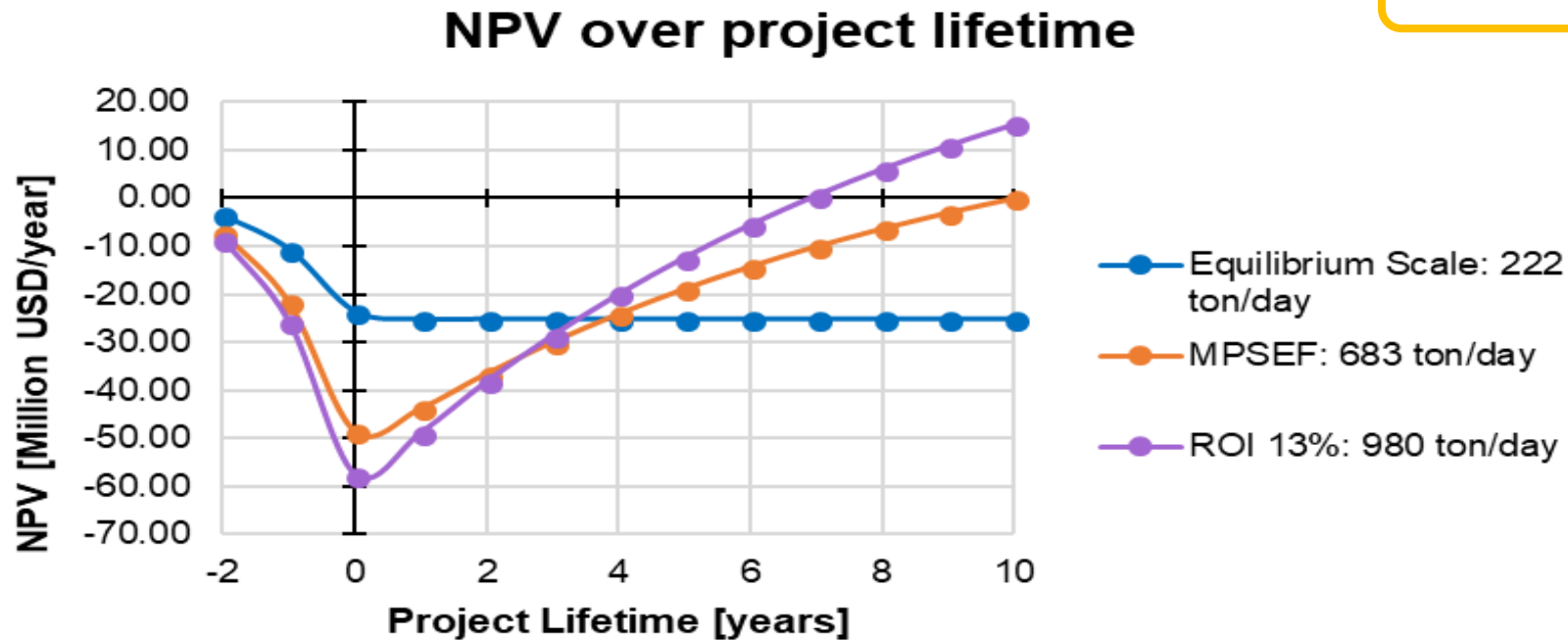


# Minimum processing scale for economic feasibility

Examples of application:

*Cocoyam-based biorefinery:*

MPSEF = 683 ton/day



# Minimum processing scale for economic feasibility

## Examples of application:

*Andes berry-based biorefinery (Dávila et al, 2016):*

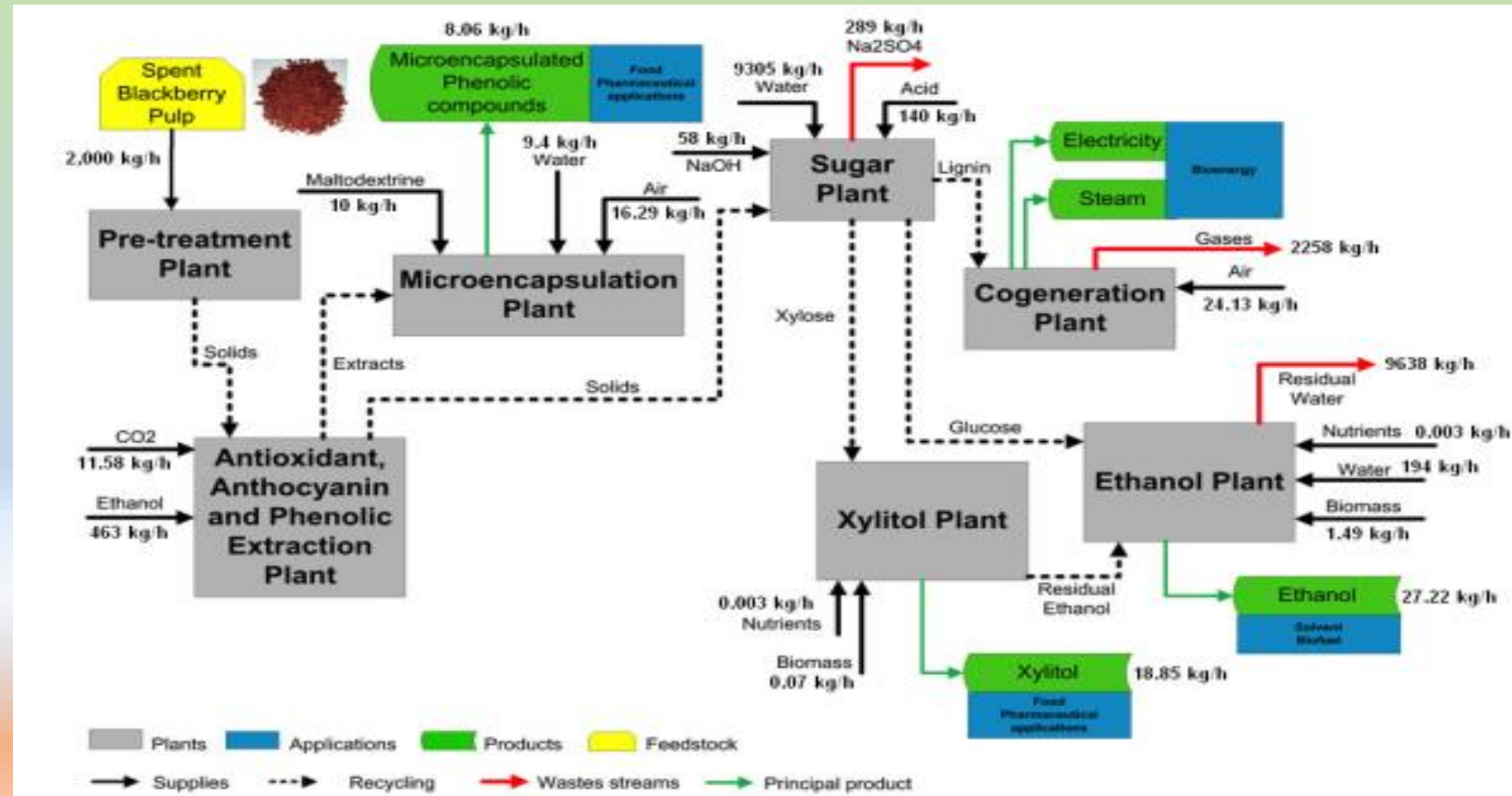
The utilization and processing chain of Andes Berry (*Rubus glaucus* benth) in Colombia is well established. The annual production of this fruit amounted to 105,285 tons that were produced on more than 10,743 ha, throughout the national territory (Ceron et al. 2012). Blackberry is commonly processed into concentrates, jams and juices (Ceron et al. 2012) and significant amounts of spent blackberry pulp (SBP) are generated as the principal residue. The blackberry fruit contains different biologically-active compounds that are desired in pharmaceutical, food and chemical applications.



# Minimum processing scale for economic feasibility

## Examples of application:

*Andes berry-based biorefinery:*

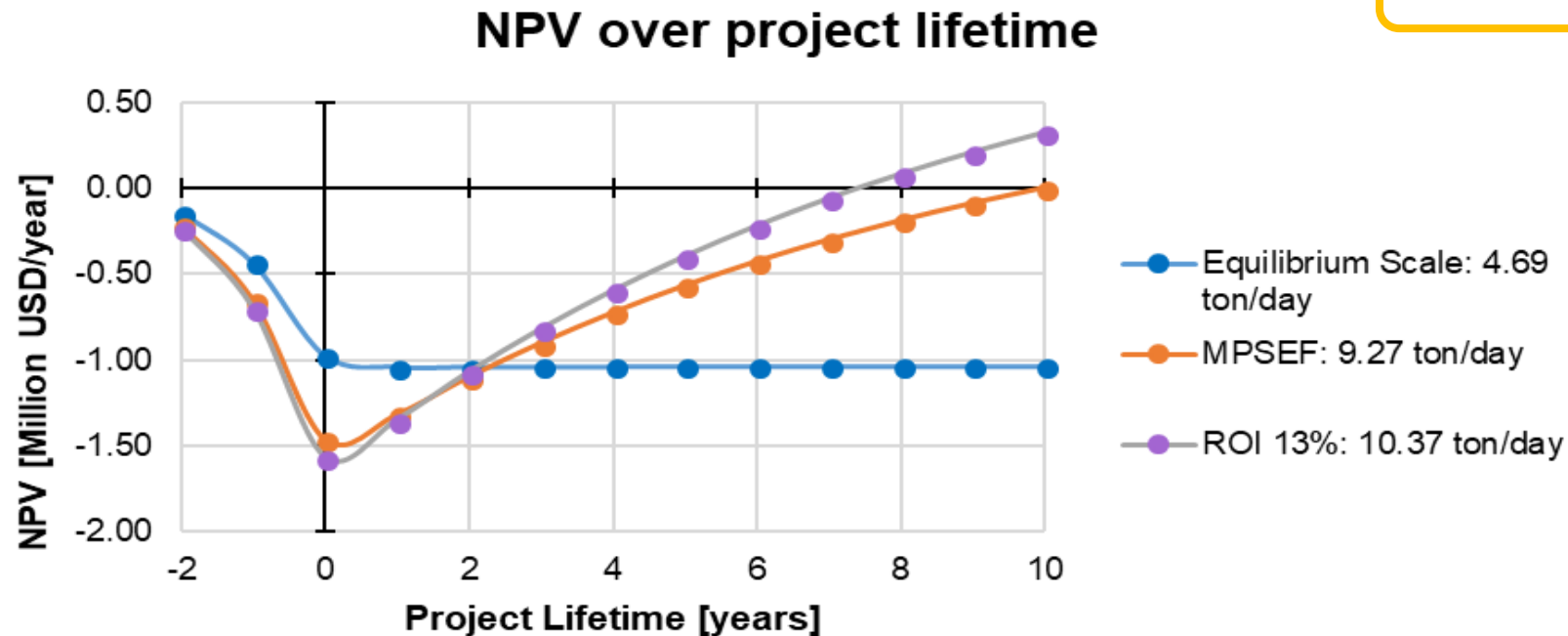


# Minimum processing scale for economic feasibility

Examples of application:

*Andes berry-based biorefinery:*

MPSEF = 9.27 ton/day



# CONCLUSIONS

To avoid surprises or risks in biorefinery projects a comprehensive analysis of the scale is needed. The knowledge based strategy is the only way to provide a real (practical ) information to be used in terms of decisions or needed changes. The theory and calculations here described could be a very cheap approximation to define the real potential of new projects especially for tropical countries. However low scale biorefineries will have always the lower value.

It is expected an increased growth in biorefinery projects at different scales during the next years depending also on oil prices. However it can be concluded that the maturity of biorefineries is still very low, even when very high developed and mature technologies are applied for ethanol or electricity production as the starting point for these biorefineries operation (not being a very sustainable biorefinery).





# Thanks for your attention

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# Referencias

- Abegunde, O.K., Mu, T.H., Chen, J.W., Deng, F.M., 2013. Physicochemical characterization of sweet potato starches popularly used in Chinese starch industry. *Food Hydrocoll.* 33, 169–177. <https://doi.org/10.1016/j.foodhyd.2013.03.005>
- Alibaba, 2017a. Calcium Hydroxide [WWW Document]. URL [https://www.alibaba.com/product-detail/Calcium-Hydroxide-Price\\_60534205666.html?s=p](https://www.alibaba.com/product-detail/Calcium-Hydroxide-Price_60534205666.html?s=p) (accessed 1.7.17).
- Alibaba, 2017b. Decanol [WWW Document]. URL [https://www.alibaba.com/product-detail/Decanol\\_1434845556.html](https://www.alibaba.com/product-detail/Decanol_1434845556.html) (accessed 1.7.17).
- Alibaba, 2017c. n-Dodecanol [WWW Document]. URL <https://www.alibaba.com/showroom/1--dodecanol.html> (accessed 1.8.17).
- Alibaba, 2017d. Alibaba - Chemicals [WWW Document]. URL [http://www.alibaba.com/Chemicals\\_p8?spm=a2700.7848340.1998821658.384.VEmQdy](http://www.alibaba.com/Chemicals_p8?spm=a2700.7848340.1998821658.384.VEmQdy) (accessed 12.1.17).
- Alibaba, 2017e. Starch [WWW Document]. URL [https://www.alibaba.com/product-detail/starch\\_273879551.html?s=p](https://www.alibaba.com/product-detail/starch_273879551.html?s=p) (accessed 1.7.17).
- Alibaba, 2017f. Xylose Syrup [WWW Document]. URL [https://www.alibaba.com/trade/search?fsb=y&IndexArea=product\\_en&CatId=&SearchText=xylose+syrup](https://www.alibaba.com/trade/search?fsb=y&IndexArea=product_en&CatId=&SearchText=xylose+syrup) (accessed 10.22.17).
- Aristizábal Marulanda, V., 2015. Jet biofuel production from agroindustrial wastes through furfural platform. Universidad Nacional de Colombia - Sede Manizales.
- Association of Official Agricultural Chemists (AOAC), 2016a. AOAC 985.29 - Total Dietary Fiber in Foods, in: Latimer, G.W.J. (Ed.), *The Official Methods of Analysis of AOAC INTERNATIONAL*. Association of Official Agricultural Chemists (AOAC).
- Association of Official Agricultural Chemists (AOAC), 2016b. AOAC 948.22 - Fat (Crude) in Nuts and Nut Products, in: Latimer, G.W.J. (Ed.), *The Official Methods of Analysis of AOAC INTERNATIONAL*. Association of Official Agricultural Chemists (AOAC).
- Cardona, C.A., 2015. Evaluación de la producción de diferentes tipos de bioenergía para uso a nivel industrial y rural, in: *II Reunión Nacional de La Red Temática En Bioenergía - XI Reunión Nacional de La REMBIO*. Ixtapa Zihuatanejo, Mexico.
- Chacón Perez, Y., Restrepo, D.L., Cardona, C.A., 2016. Comparison of cassava and sugarcane bagasse for fuel ethanol production, in: Klein, C. (Ed.), *Handbook on Cassava: Production, Potential Uses and Recent Advances*. Nova Publishers, New York, pp. 1–28.
- De Jong, E., Higson, A., Walsh, P., Wellisch, M., 2012. Bio-based Chemicals: Value Added Products from Biorefineries.
- Dubois, M., Gilles, K.A., Hamilton, J.K., Rebers, P.A., Smith, F., 1956. Phenol Sulphuric Acid Method for Total Carbohydrate. *Anal. Chem.* 26, 350.
- Forero Hernández, H.A., 2015. Practical Application of Thermodynamics in the Optimal Synthesis of Chemical and Biotechnological Processes. Universidad Nacional de Colombia - Sede Manizales.
- Gómez Z., M.E., 2003. Una revisión sobre el Bore (Alocasia macrorrhiza), in: *Agroforestería Para La Producción Animal En América Latina-II*. Colección FAO, Rome, pp. 203–212.
- Gutiérrez, L.F., Sánchez, Ó.J., Cardona, C.A., 2013. Analysis and design of extractive fermentation processes using a novel short-cut method. *Ind. Eng. Chem. Res.* 52, 12915–12926. <https://doi.org/10.1021/ie301297h>
- Han, J.S., Rowell, J.S., 1996. Chemical Composition of Fibers, in: Rowell, R.M., Young, R.A., Rowell, J.K. (Eds.), *Paper and Composites from Agro-Based Resources*. CRC Press, New York.
- Hoover, R., Ratnayake, W.S., 2001. Determination of total amylose content of starch, in: *Current Protocols in Food Analytical Chemistry*. John Wiley & Sons, Inc. <https://doi.org/10.1002/0471142913.fae0203s00>
- Jin, Q., Zhang, H., Yan, L., Qu, L., Huang, W., 2011. Kinetic characterization for hemicellulose hydrolysis of corn stover in a dilute acid cycle spray flow through reactor at moderate conditions. *Biomass and Bioenergy* 35(10), 4158–64.
- Krishnaveni, S., Sadavisam, S., Balasubramanian, T., 1984. Phenol Sulphuric Acid Method for Total Carbohydrate. *Food Chem.* 15, 229.
- Min, D.-J., Choi, K.H., Chang, Y.K., Kim, J.-H., 2011. Effect of operating parameters on precipitation for recovery of lactic acid from calcium lactate fermentation broth. *Korean J. Chem. Eng.* 28, 1969–1974.



# Referencias

- Ministerio de Agricultura y Desarrollo Rural, 2018. Red de Información y Comunicación del Sector Agropecuario Colombiano [WWW Document]. Estadísticas - Agrícola. URL <http://www.agronet.gov.co/estadistica/Paginas/default.aspx> (accessed 1.5.18).
- Moncada, J., Cardona, C.A., Higueta, J.C., Vélez, J.J., López-Suarez, F.E., 2016. Wood residue (Pinus patula bark) as an alternative feedstock for producing ethanol and furfural in Colombia: Experimental, techno-economic and environmental assessments. *Chem. Eng. Sci.* 140, 309–318. <https://doi.org/10.1016/j.ces.2015.10.027>
- Moncada, J., Tamayo, J., Cardona, C.A., 2014. Evolution from biofuels to integrated biorefineries: Techno-economic and environmental assessment of oil palm in Colombia. *J. Clean. Prod.* 81, 51–59. <https://doi.org/10.1016/j.jclepro.2014.06.021>
- Moncada B., J., Aristizábal M., V., Cardona A., C.A., 2016. Design strategies for sustainable biorefineries. *Biochem. Eng. J.* 116, 122–134. <https://doi.org/10.1016/j.bej.2016.06.009>
- Montoya Henao, S., 2007. Obtención de almidón nativo y sus aplicaciones. Cali.
- Morales-Rodriguez, R., Gernaey, K. V., Meyer, A.S., Sin, G., 2011. A Mathematical model for simultaneous saccharification and co-fermentation (SSCF) of C6 and C5 sugars. *Chinese J. Chem. Eng.* 19, 185–191. [https://doi.org/10.1016/S1004-9541\(11\)60152-3](https://doi.org/10.1016/S1004-9541(11)60152-3)
- Olaleye-Lydia, D., Owolabi-Bodunde, J., Adesina-Adeniyi, O., Isiaka-Adekunle, A., 2013. Chemical Composition of Red and White Cocoyam (Colocasia esculenta) Leaves. *Int. J. Sci. Res.* 2, 121–126.
- Owusu-Darko, P.G., Paterson, A., Omenyo, E.L., 2014. Cocoyam (corms and cormels)—An underexploited food and feed resource. *J. Agric. Chem. Environ.* 3, 22–29. <https://doi.org/10.4236/jacen.2014.31004>
- Peters, M.S., Timmerhaus, K.D., West, R.E., 1991. Chapter 6: Cost Estimation, in: *Plant Design and Economics for Chemical Engineers*. p. 923.
- Pleissner, D., Demichelis, F., Mariano, S., Fiore, S., Navarro Gutiérrez, I.M., Schneider, R., Venus, J., 2017. Direct production of lactic acid based on simultaneous saccharification and fermentation of mixed restaurant food waste. *J. Clean. Prod.* 143, 615–623. <https://doi.org/10.1016/j.jclepro.2016.12.065>
- Rivera, E.C., Costa, A.C., Atala, D.I.P., Maugeri, F., Maciel, M.R.W., Filho, R.M., 2006. Evaluation of optimization techniques for parameter estimation: application to ethanol fermentation considering the effect of temperature. *Process Biochem.* 41, 1682–1687.
- Selig, M.J., Weiss, N., Ji, Y., 2008. Enzymatic Saccharification of Lignocellulosic Biomass, Technical Report NREL/TP-510-42629.
- Serna Loaiza, S., Posada Bedoya, S., 2014. Sorbitol production from the “mafafa”, root of the plant named “bore” or “oreja de elefante.” Universidad Nacional de Colombia.
- Siqueira, P.F., Karp, S.G., Carvalho, J.C., Sturm, W., Rodríguez-León, J.A., Tholozan, J.L., Singhania, R.R., Pandey, A., Soccol, C.R., 2008. Production of bio-ethanol from soybean molasses by *Saccharomyces cerevisiae* at laboratory, pilot and industrial scales. *Bioresour. Technol.* 99, 8156–8163. <https://doi.org/10.1016/j.biortech.2008.03.037>
- Sluiter, A., Hames, B., Ruiz, R., Scarlata, C., Sluiter, J., Templeton, D., 2008. Technical Report NREL/TP-510-42622: Determination of Ash in Biomass. Golden, Colorado.
- Sun, Y., Cheng, J., 2002. Hydrolysis of lignocellulosic materials for ethanol production: A review. *Bioresour. Technol.* 83, 1–11. [https://doi.org/10.1016/S0960-8524\(01\)00212-7](https://doi.org/10.1016/S0960-8524(01)00212-7)
- Ulrich, G.D., Vasudevan, P.T., 2006. How to estimate utility costs. *Chem. Eng.* 113, 66–69.
- Valcárcel-Yamani, B., Rondán-Sanabria, G.G., Finardi-Filho, F., 2013. The physical, chemical and functional characterization of starches from andean tubers: Oca (*Oxalis tuberosa* molina), olluco (*Ullucus tuberosus* caldas) and mashua (*Tropaeolum tuberosum* ruiz & pavón). *Brazilian J. Pharm. Sci.* 49, 453–464. <https://doi.org/10.1590/S1984-82502013000300007>
- Virunanon, C., Ouephanit, C., Burapatana, V., Chulalaksananukul, W., 2013. Cassava pulp enzymatic hydrolysis process as a preliminary step in bio-production from waste starchy resources. *J. Clean. Prod.* 39, 273–279.
- Zhang, M., Xie, L., Yin, Z., Khanal, S.K., Zhou, Q., 2016. Biorefinery approach for cassava-based industrial wastes: Current status and opportunities. *Bioresour. Technol.* 215, 50–62. <https://doi.org/10.1016/j.biortech.2016.04.026>

